

# Kemijsko inženjerska termodinamika

Numeričke vježbe

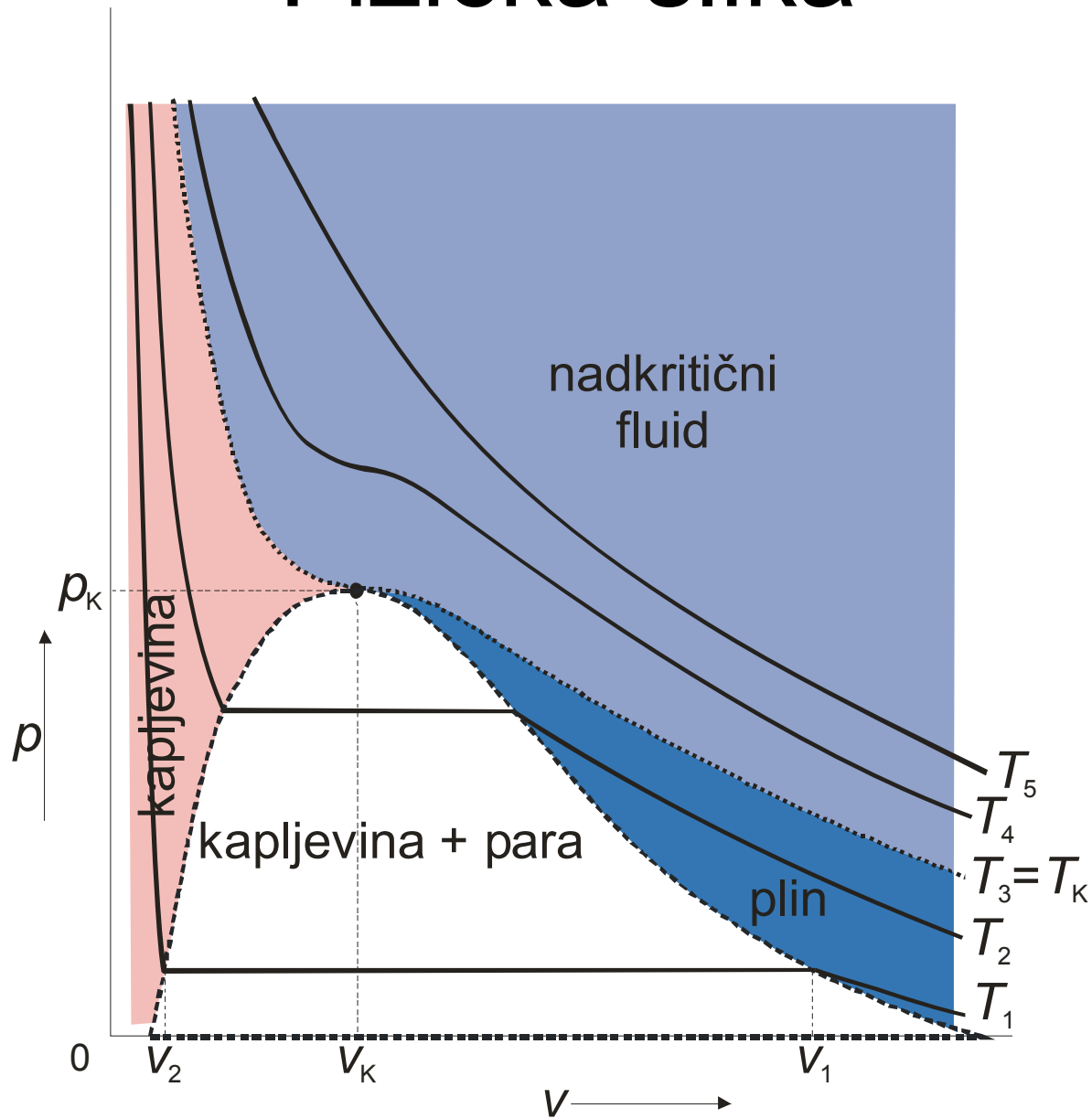
I. zadatak

# Umjesto uvoda

**"Thermodynamics is a funny subject. The first time you go through it, you don't understand it at all. The second time you go through it, you think you understand it, except for one or two small points. The third time you go through it, you know you don't understand it, but by that time you are so used to it, it doesn't bother you any more."**

**- Arnold Sommerfield**

# Fizička slika



# Jednadžbe stanja III. stupnja

Virijalna 
$$v^3 - \frac{RT}{p}v^2 - \frac{B(T)RT}{p}v - \frac{C(T)RT}{p} = 0$$

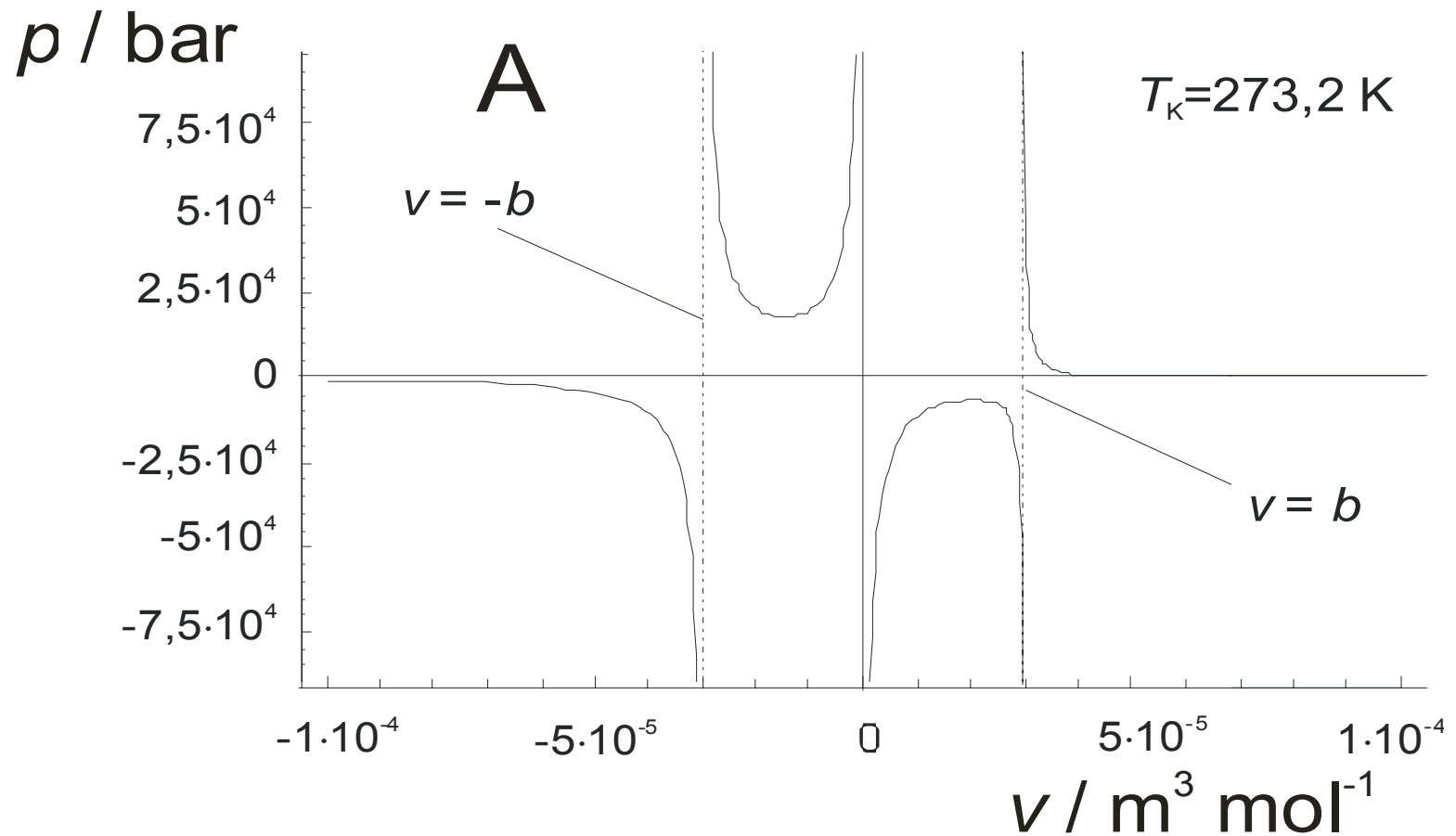
van der Waals 
$$v^3 - v^2\left(b + \frac{RT}{p}\right) + v\left(\frac{a}{p}\right) - \frac{ab}{p} = 0$$

Redlich Kwong 
$$v^3 - \frac{RT}{p}v^2 - \left(b^2 + \frac{RTb}{p} - \frac{a}{p\sqrt{T}}\right)v - \frac{ab}{p\sqrt{T}} = 0$$

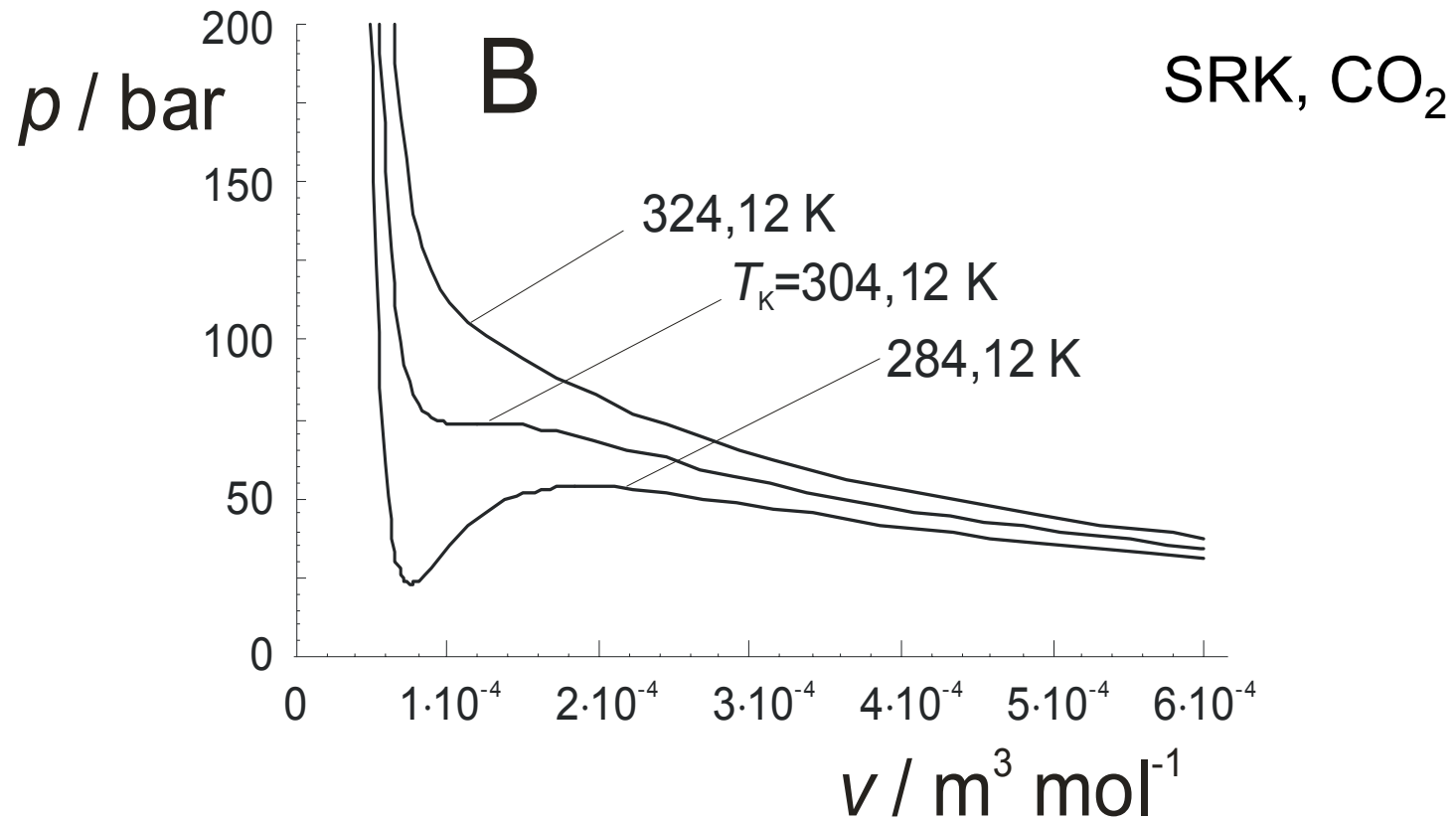
SRK 
$$v^3 - \frac{RT}{p}v^2 - \left(b^2 + \frac{RTb}{p} - \frac{a\alpha}{p}\right)v - \frac{a\alpha b}{p} = 0$$

PR 
$$v^3 - \left(\frac{RT}{p} - b\right)v^2 - \left(3b^2 + \frac{2RTb}{p} - \frac{a\alpha}{p}\right)v - \left(\frac{a\alpha b}{p} - \frac{RTb^2}{p} - b^3\right) = 0$$

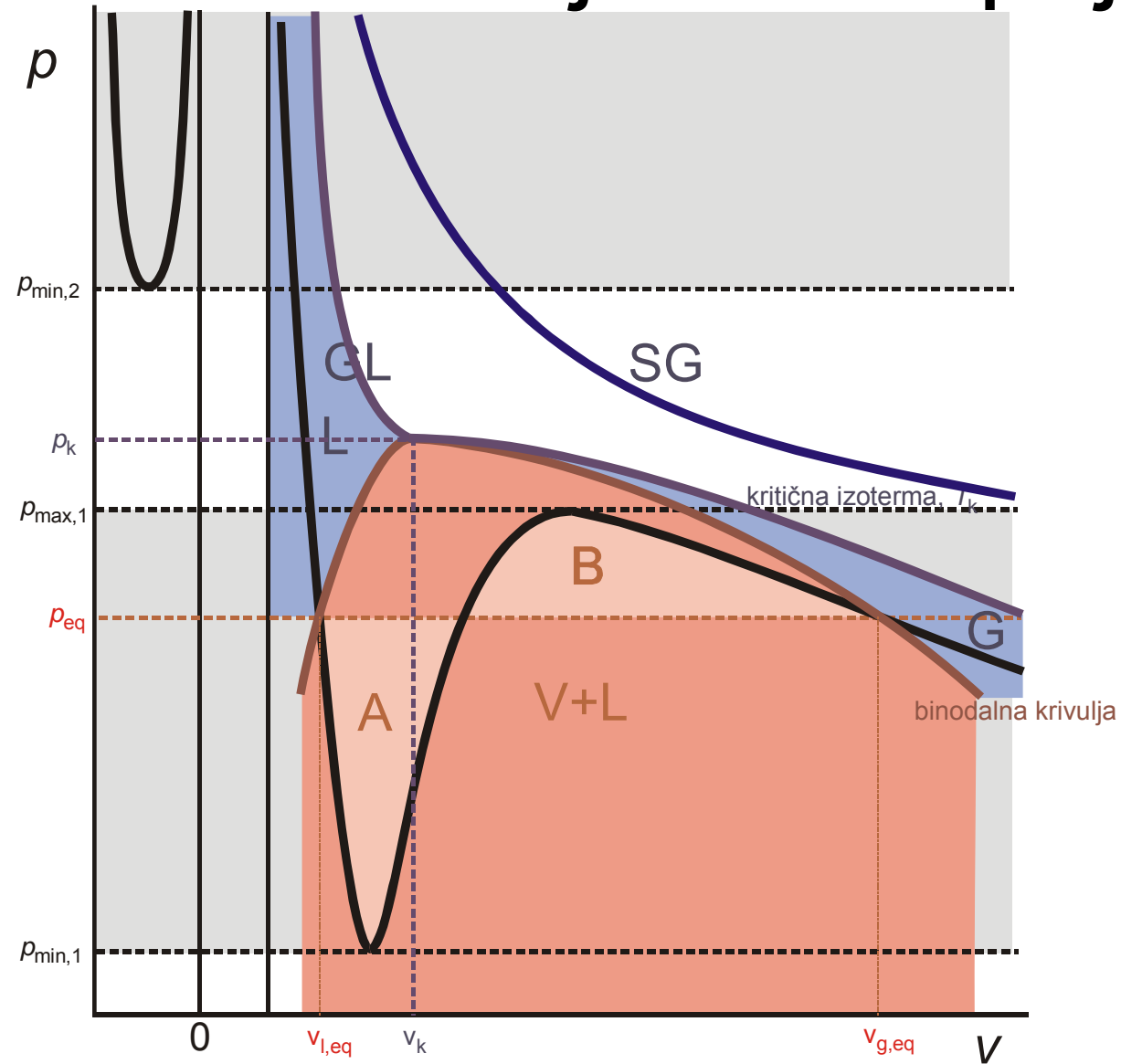
# Jednadžbe stanja III. stupnja



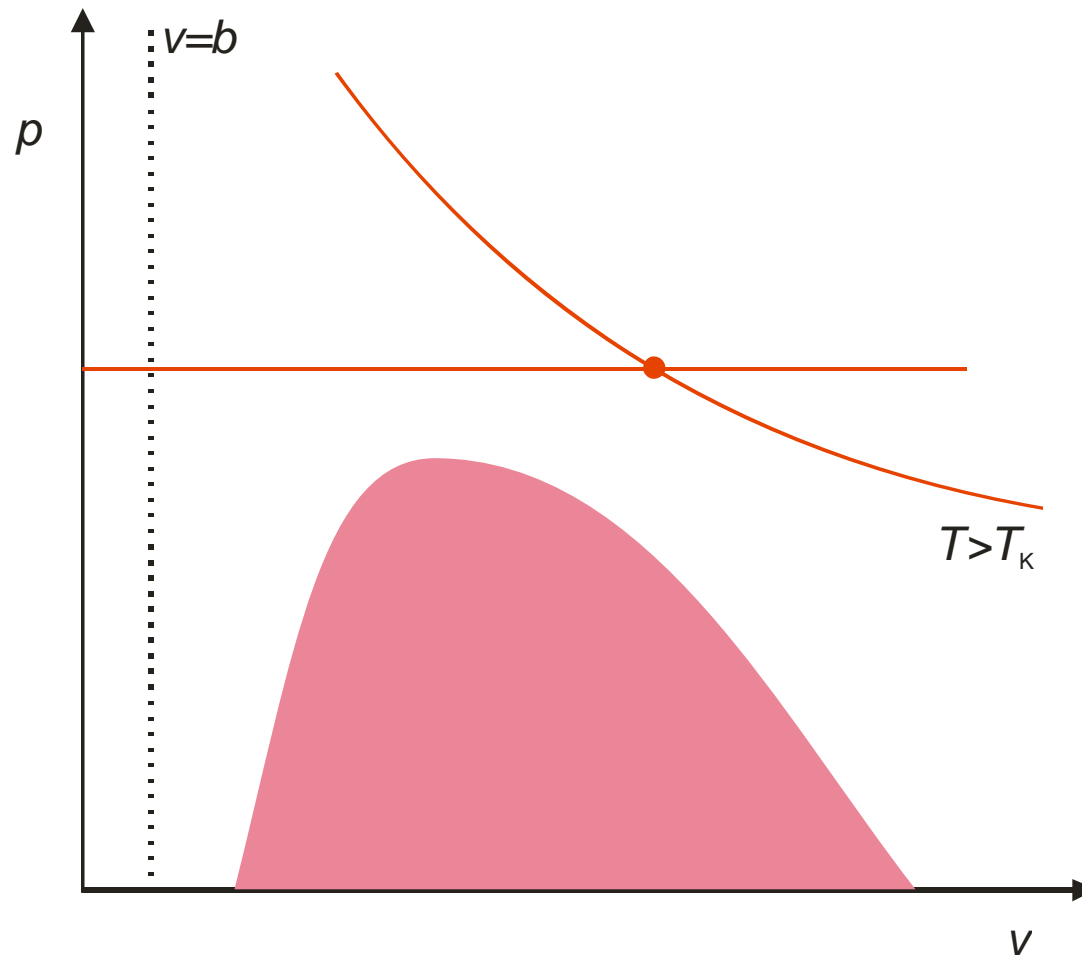
# Jednadžbe stanja III. stupnja



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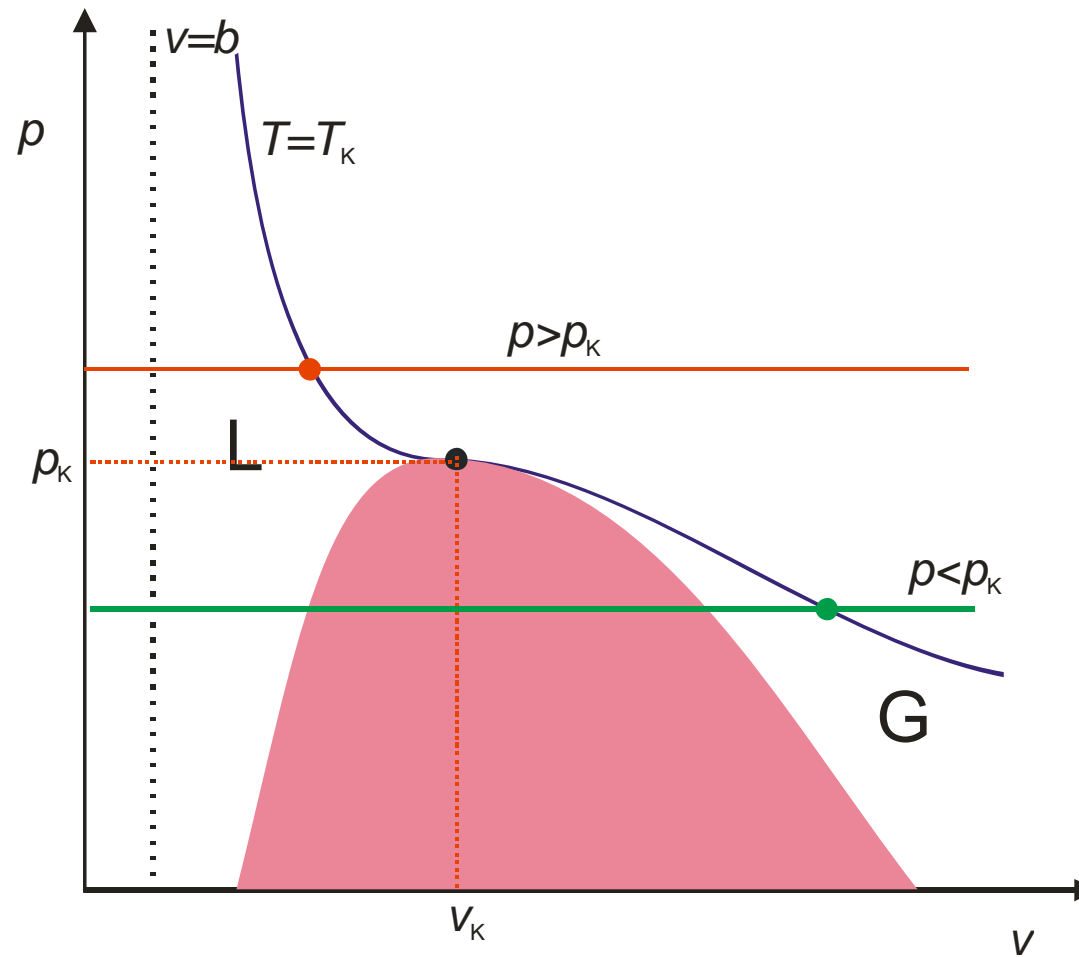


# Jednadžbe stanja III. stupnja

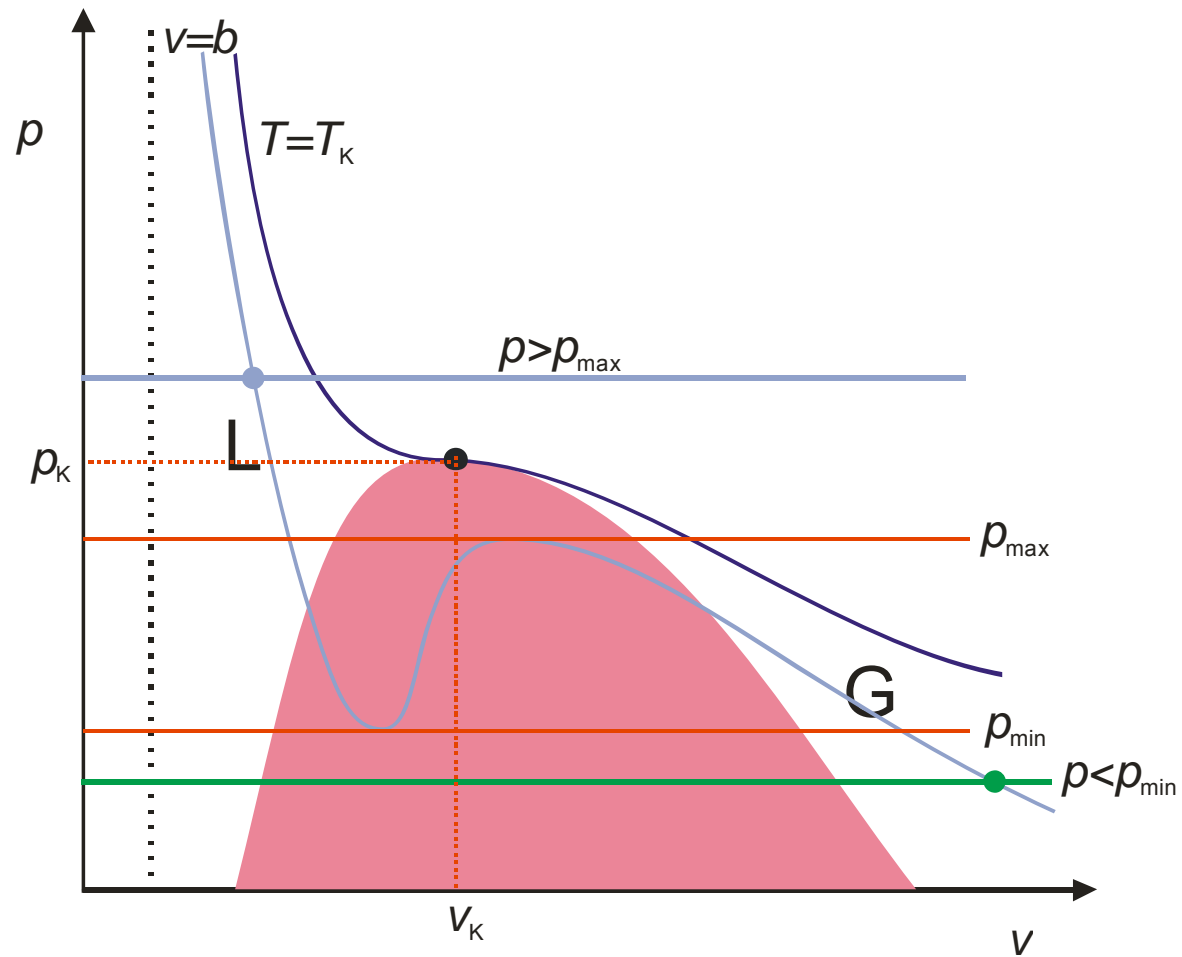




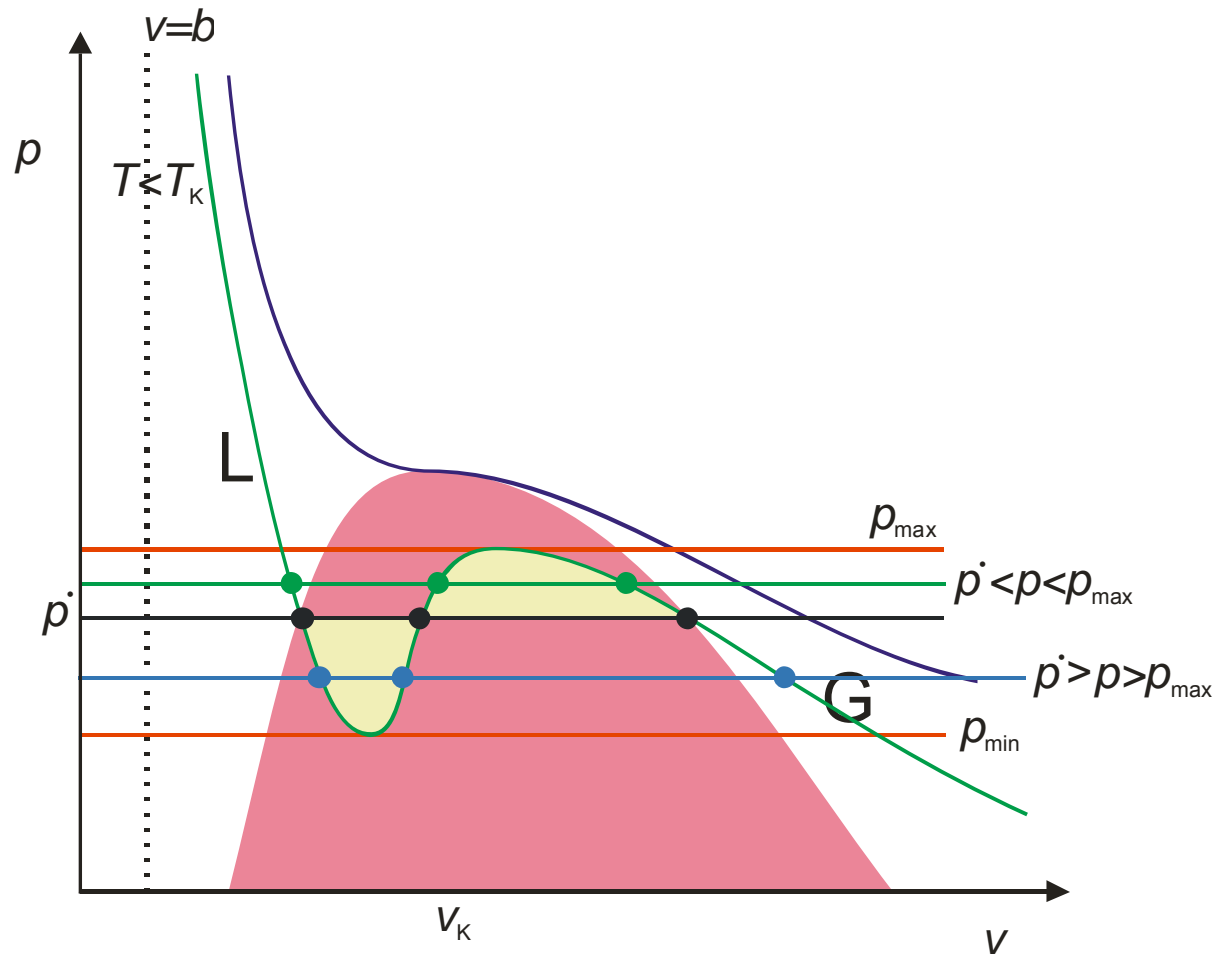
# Jednadžbe stanja III. stupnja



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# Jednadžbe stanja III. stupnja



# Jednadžbe stanja III. stupnja

$$v = \frac{zRT}{p}$$

$$\text{RK} \quad z^3 - z^2 - \left( \frac{b^2 p^2}{R^2 T^2} + \frac{pb}{RT} - \frac{ap}{R^2 T^2 \sqrt{T}} \right) z - \frac{abp^2}{R^3 T^3 \sqrt{T}} = 0$$

$$\text{SRK} \quad z^3 - z^2 - \left( \frac{b^2 p^2}{R^2 T^2} + \frac{bp}{RT} - \frac{a\alpha p}{R^2 T^2} \right) z - \frac{a\alpha bp^2}{R^3 T^3} = 0$$

$$\text{PR} \quad z^3 - \left( 1 - \frac{bp}{RT} \right) z^2 - \left( \frac{3b^2 p^2}{R^2 T^2} + \frac{2bp}{RT} - \frac{a\alpha p}{R^2 T^2} \right) z - \left( \frac{a\alpha bp^2}{R^3 T^3} - \frac{b^2 p^2}{R^2 T^2} - \frac{b^3 p^3}{R^3 T^3} \right) = 0$$

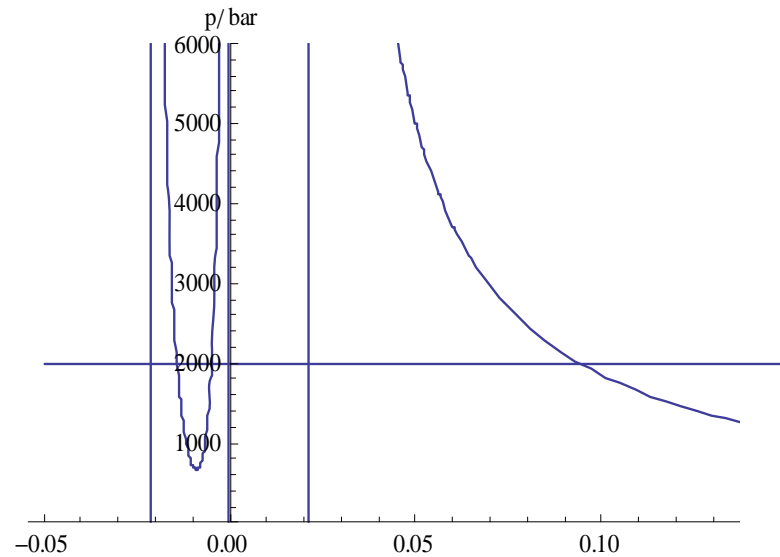
# Jednadžbe stanja III. stupnja

RK  $z^3 - z^2 + (A - B^2 - B)z - AB = 0$

SRK  $z^3 - z^2 + (A - B^2 - B)z - AB = 0$

PR  $z^3 - (1 - B)z^2 + (A - 3B^2 - 2B)z - (AB - B^2 - B^3) = 0$

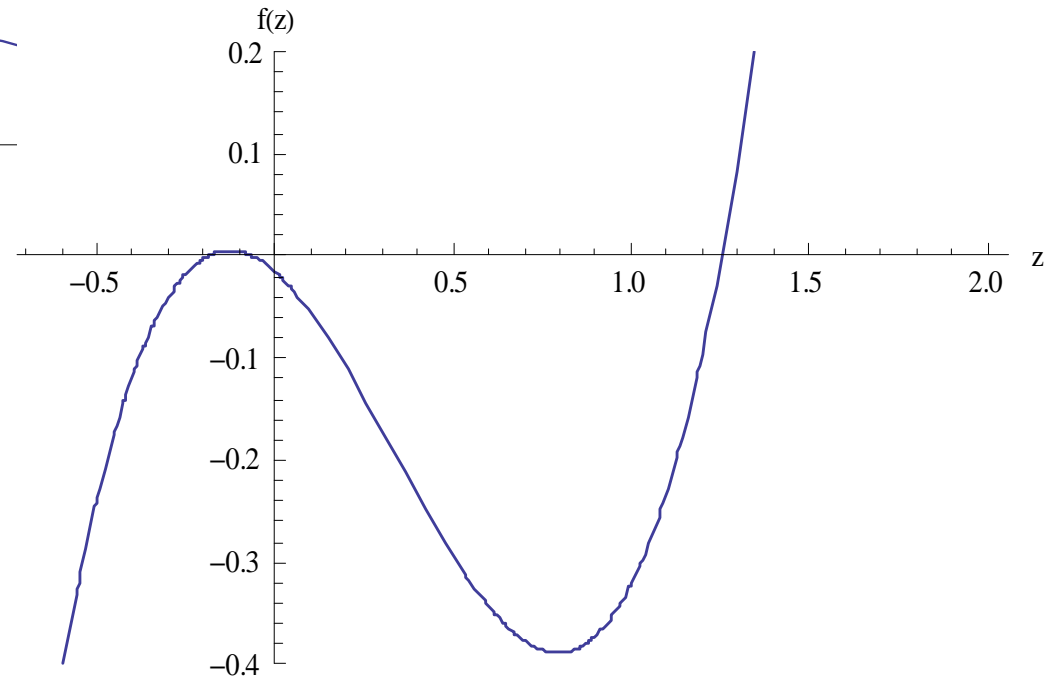
# Jednadžbe stanja III. stupnja



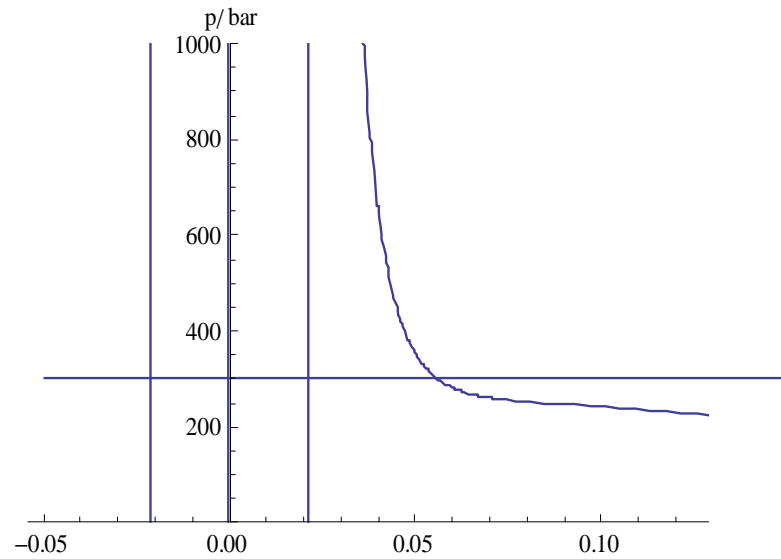
Voda, SRK

Temperature iznad kritične  
Vrlo visoki tlakovi

Jednadžbe stanja III stupnja nisu  
pogodne za područje visokih temperatura  
i tlakova

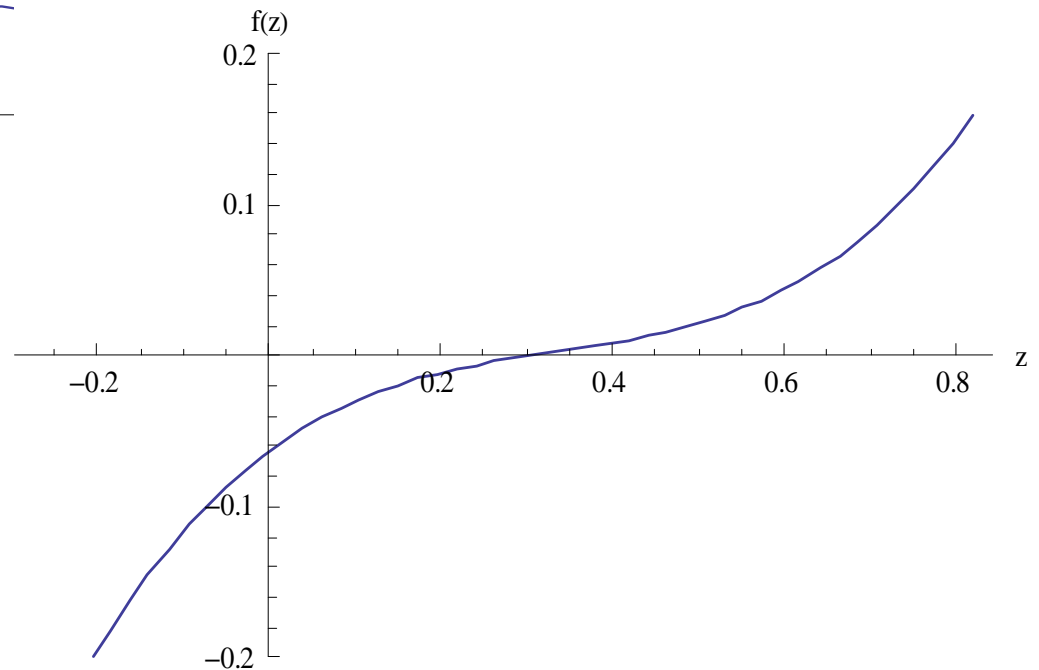


# Jednadžbe stanja III. stupnja

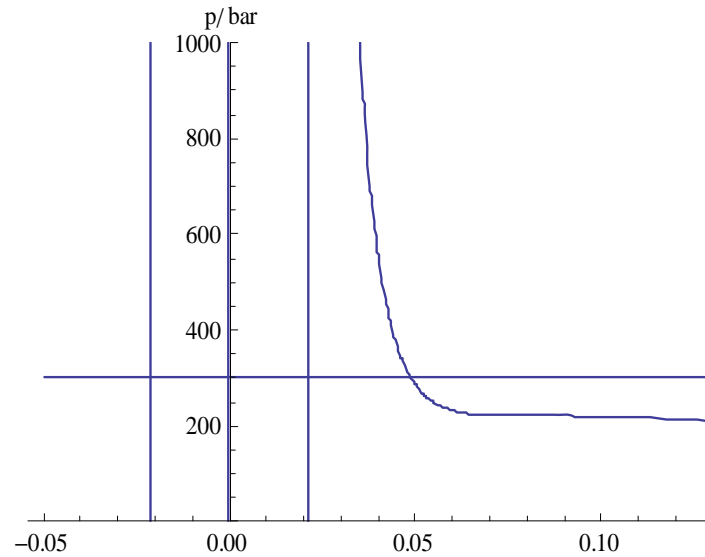


Voda, SRK

Temperature iznad kritične  
Niži tlakovi

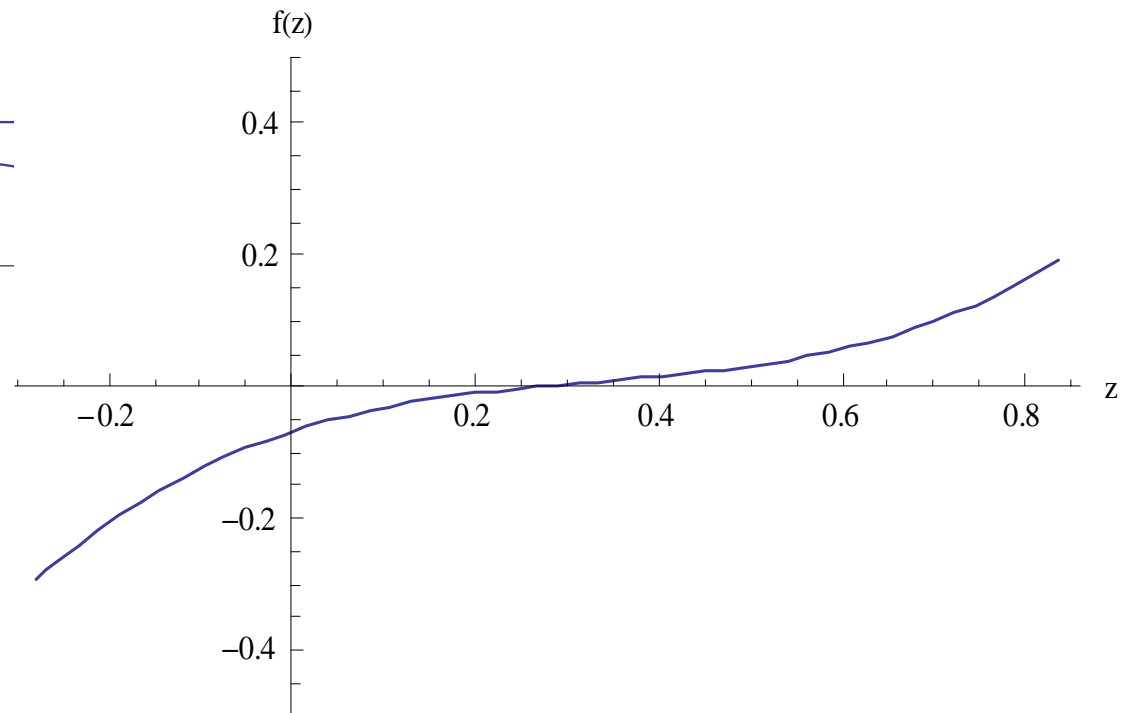


# Jednadžbe stanja III. stupnja



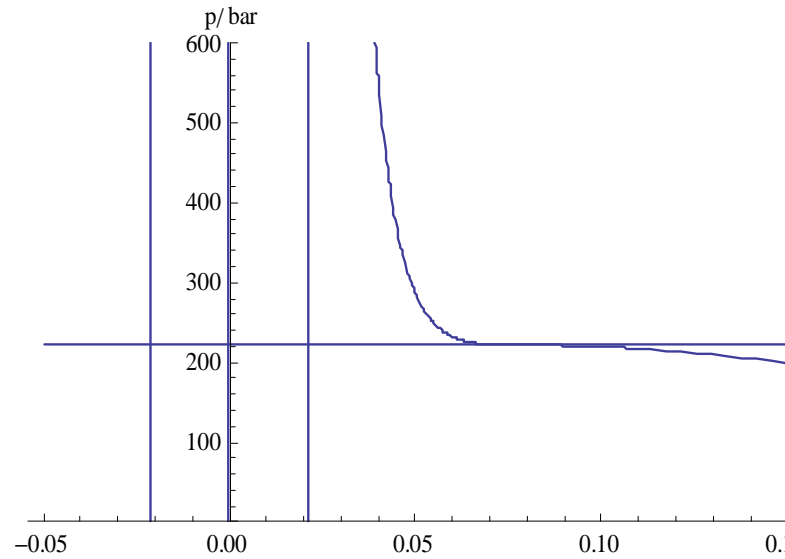
Voda, SRK

Kritična temperatura  
Visoki (ali ne previsoki) tlakovi



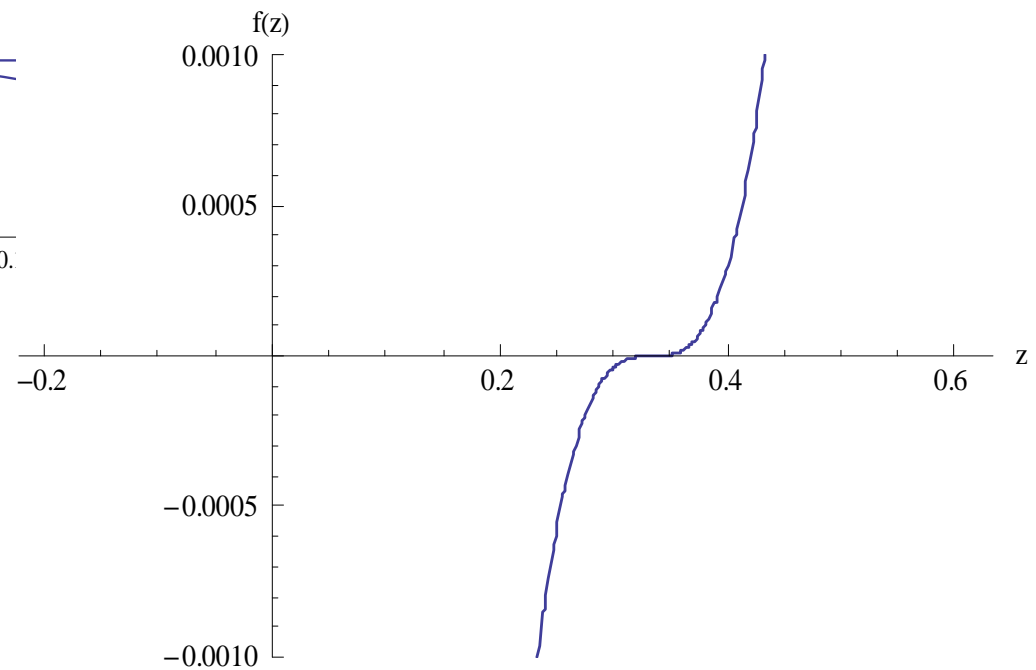


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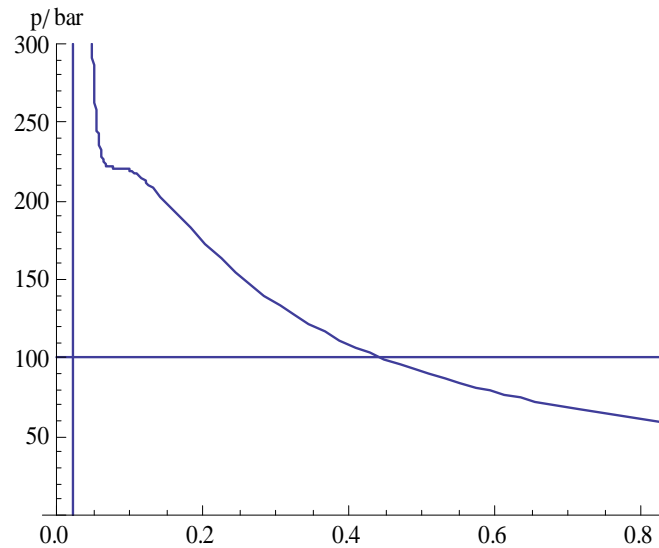


Voda, SRK

Kritična temperatura  
Kritični tlak

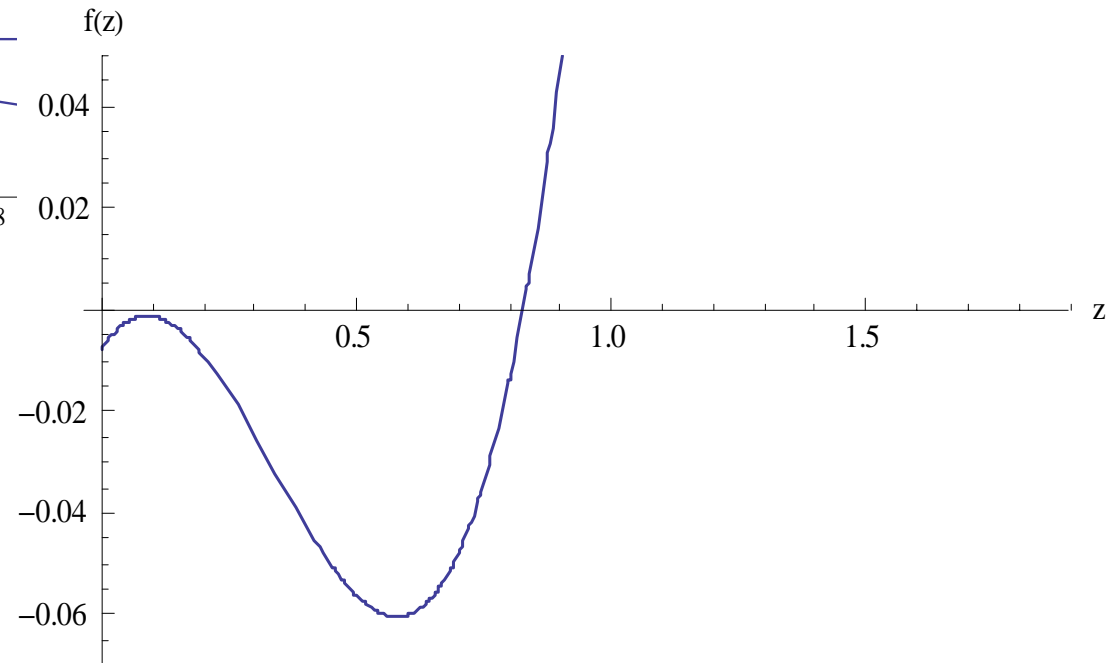


# Jednadžbe stanja III. stupnja

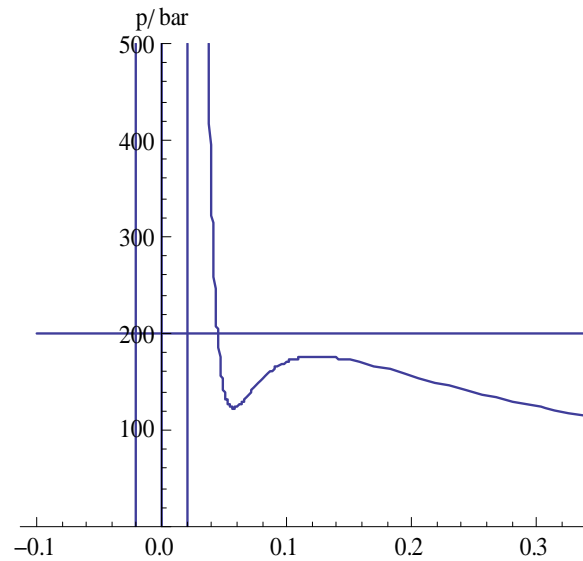


Voda, SRK

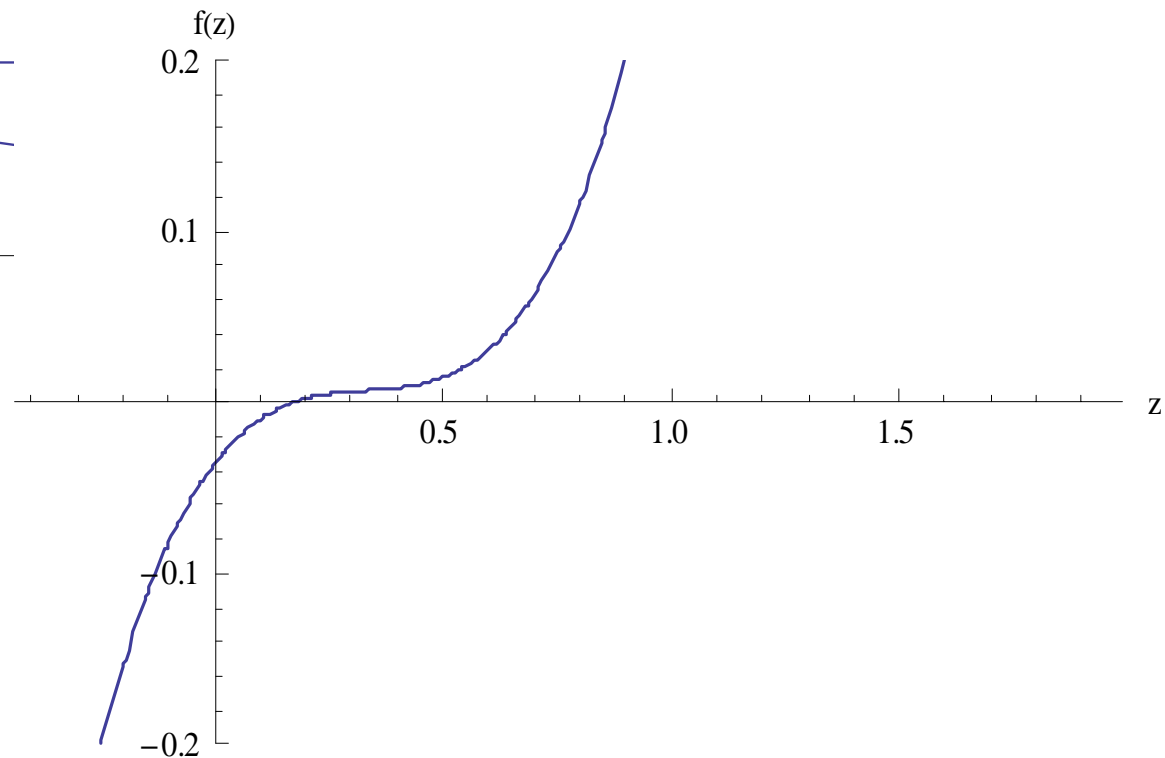
Kritična temperatura  
Tlak ispod kritičnog



# Jednadžbe stanja III. stupnja

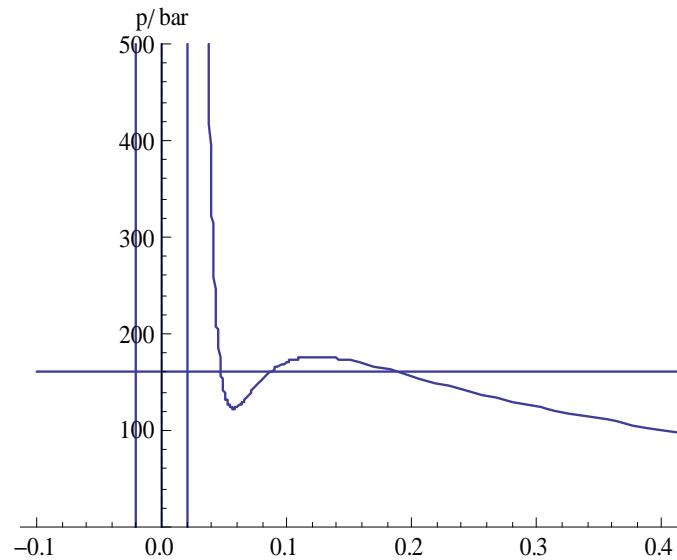


Subkritična temperatura  
Tlak veći od  $p_{\max}$ ,  
Visok (ali ne previsok)



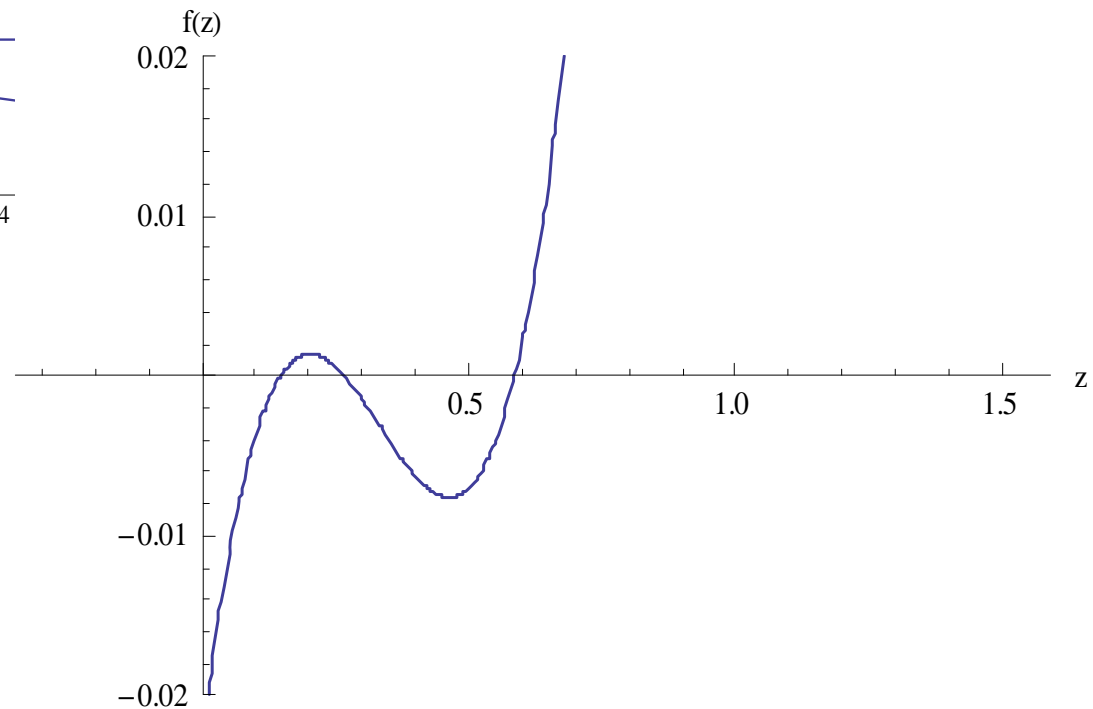
Voda, SRK

# Jednadžbe stanja III. stupnja

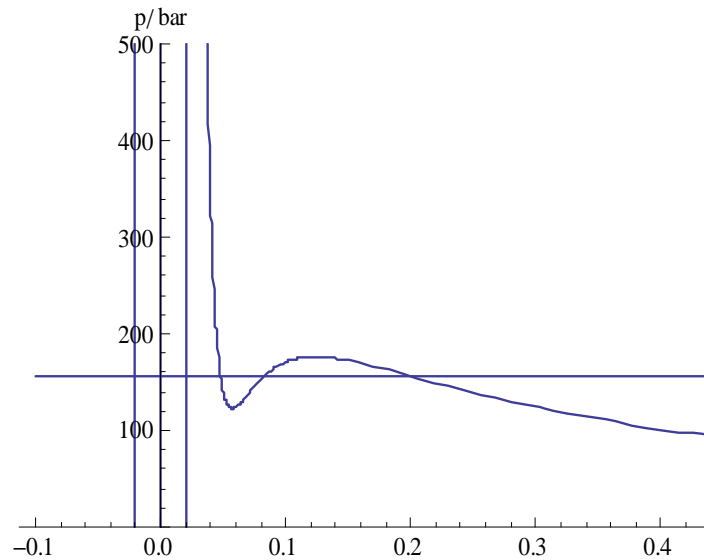


Voda, SRK

Subritična temperatura  
Tlak veći od ravnotežnog  
Tlak manji od  $p_{\max}$

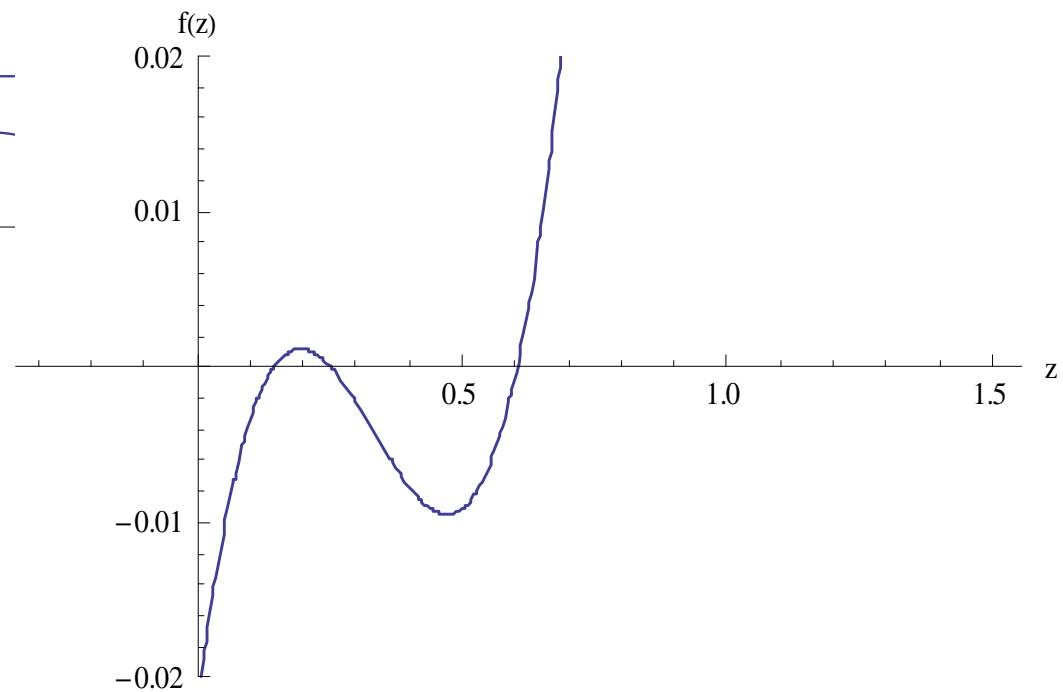


# Jednadžbe stanja III. stupnja

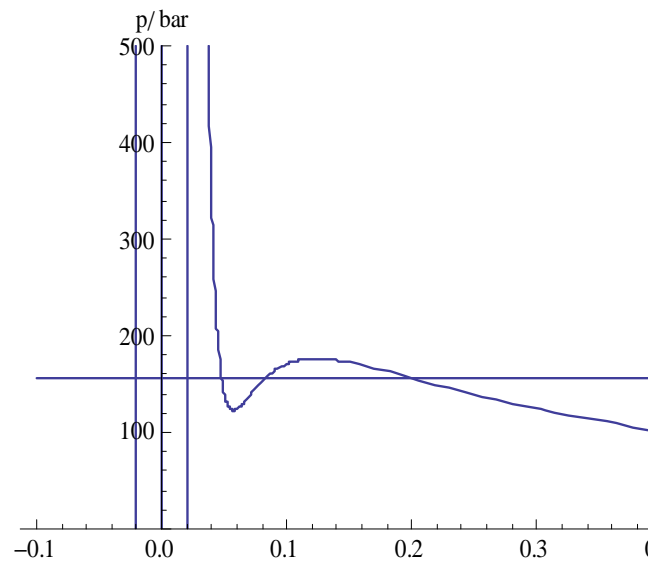


Voda, SRK

Subritična temperatura  
Tlak jednak ravnotežnom

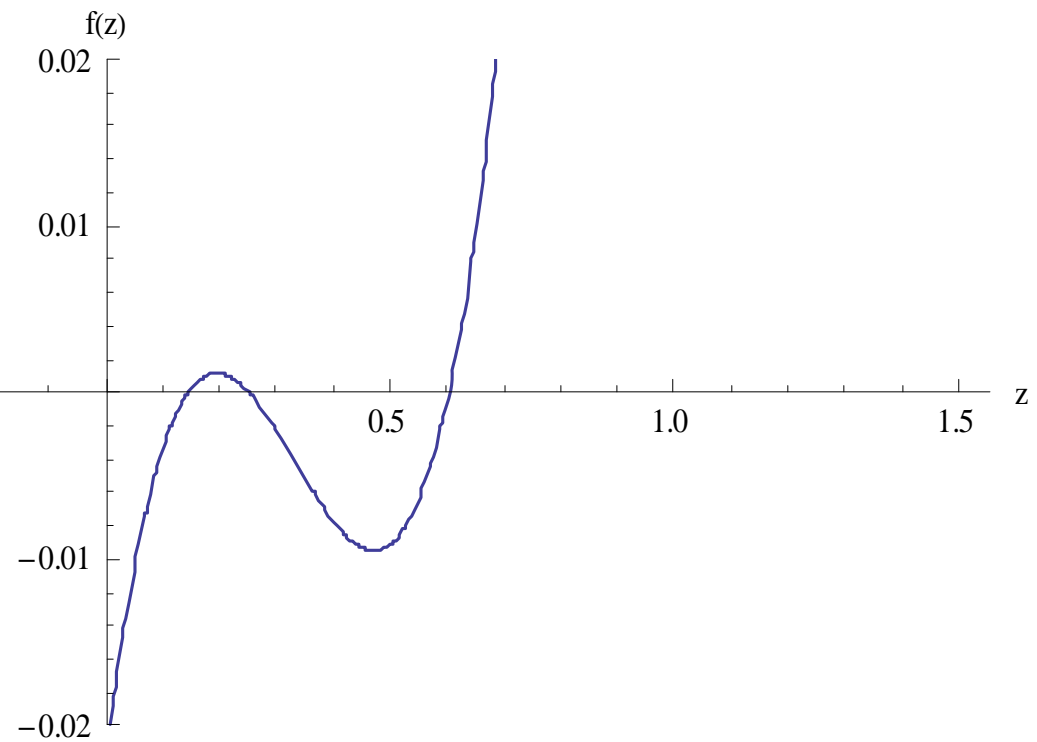


# Jednadžbe stanja III. stupnja

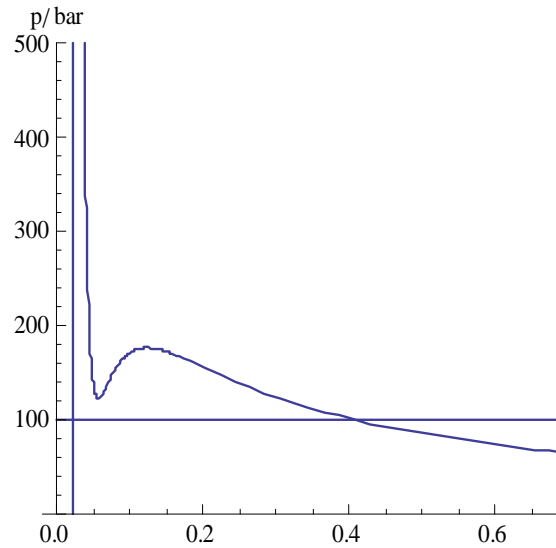


Voda, SRK

Subritična temperatura  
Tlak manji od ravnotežnog  
Tlak veći od  $p_{\min}$

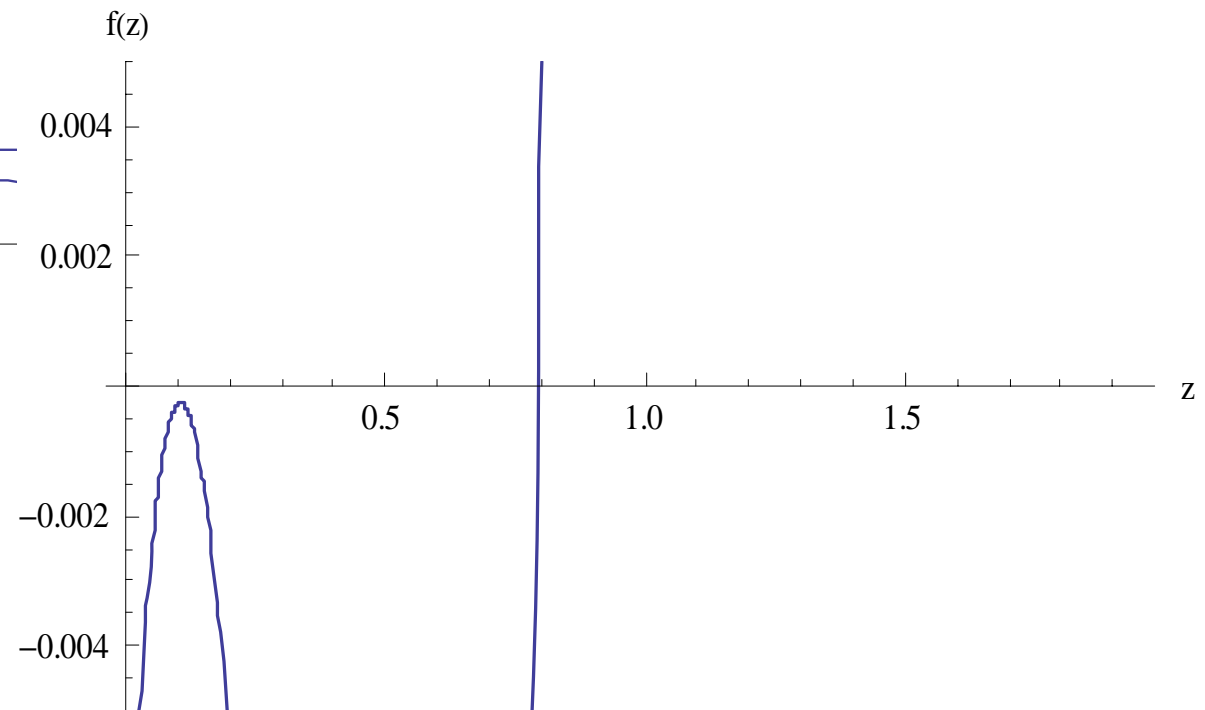


# Jednadžbe stanja III. stupnja



Voda, SRK

Subritična temperatura  
Tlak manji od od  $p_{\min}$

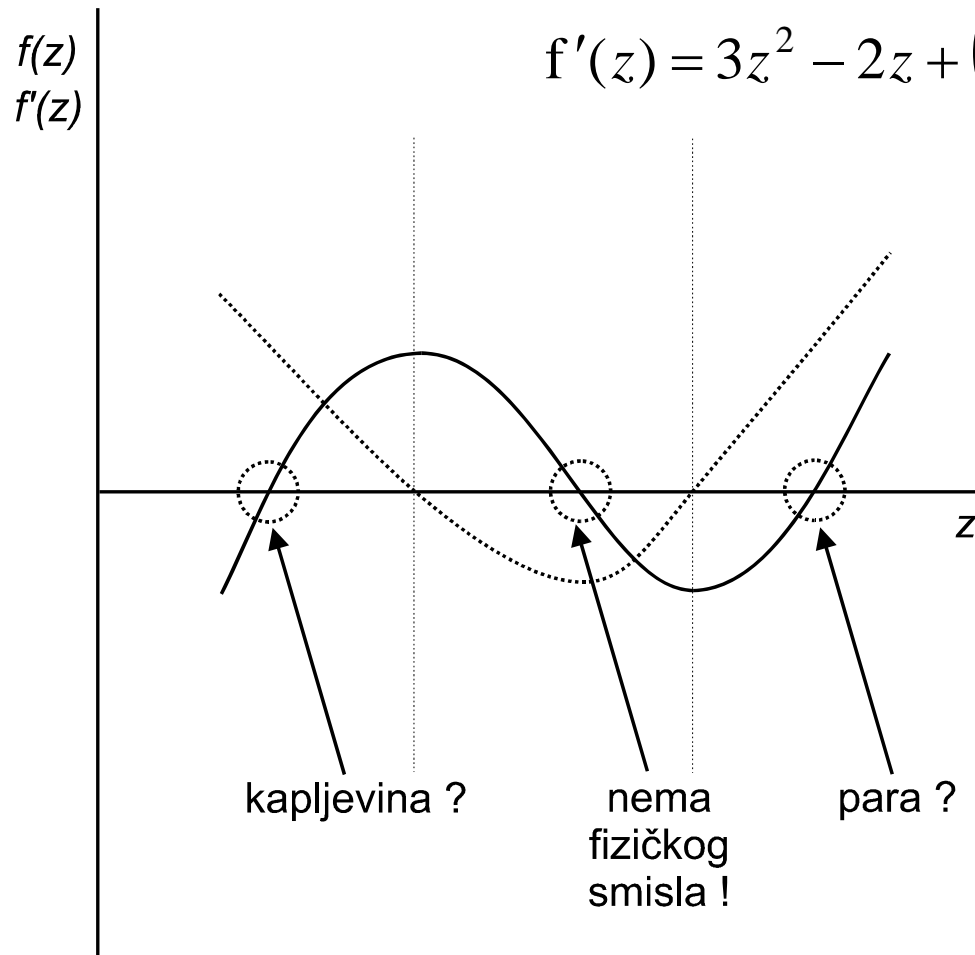


# Način rješavanja

Soave Redlich Kwong

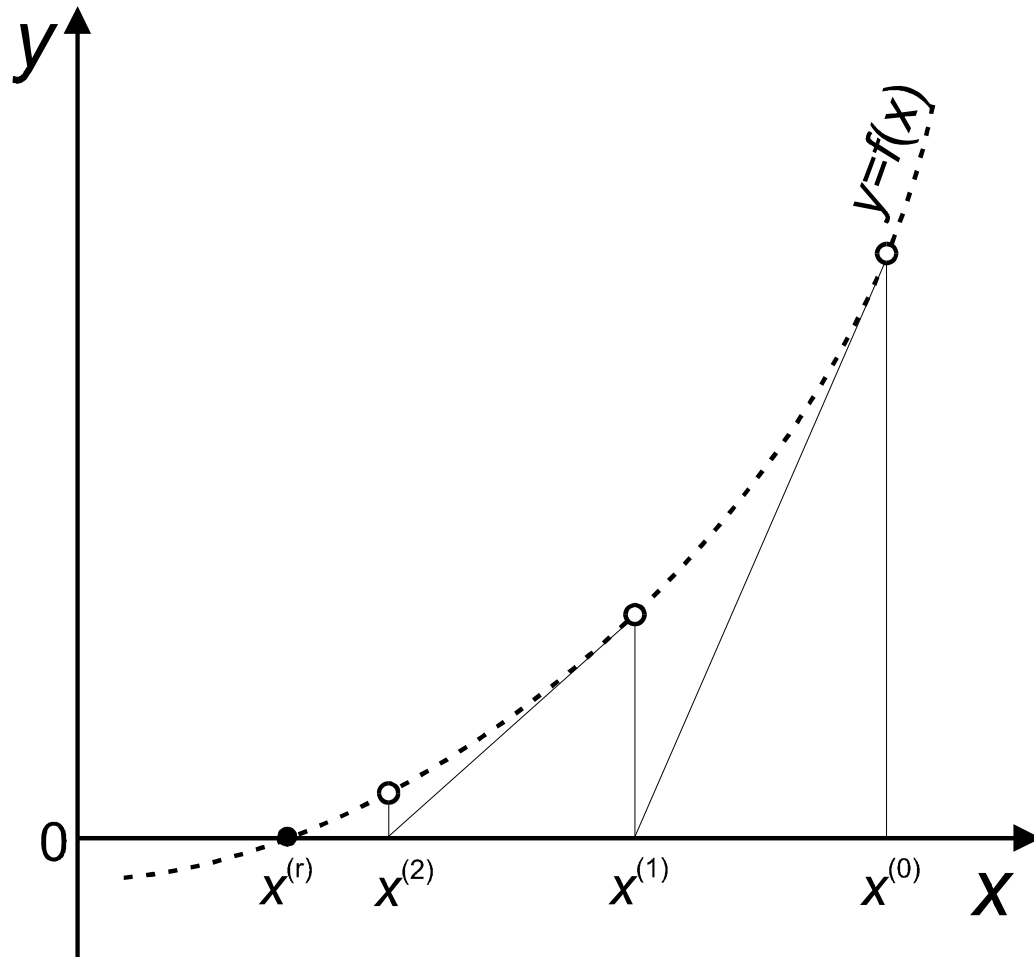
$$f(z) = z^3 - z^2 + (A - B^2 - B)z - AB = 0$$

$$f'(z) = 3z^2 - 2z + (A - B^2 - B) = 0$$





# Način rješavanja



$$f(x) = 0$$

$$x^{(i+1)} = x^{(i)} - \frac{f(x^{(i)})}{f'(x^{(i)})}$$

# Način rješavanja

Izbor početnih pretpostavki

kapljevina  $z_0 = B$   $B = \frac{pb}{RT} = \frac{b}{v^{\text{id}}}$

para  $z_0 = 1$   $z = \frac{pv}{RT} = \frac{v}{v^{\text{id}}}$

# Primjer zadatka

## Zadatak 1 – primjer.

Za smjesu *propan(1) – n-butan (2) – i-butan(3)* molarnih udjela  $y_1 = 0.4$ ,  $y_2 = 0.25$  izračunati koeficijent kompresibilnosti i molarni volumen pri sljedećim uvjetima:

a)  $p = \underline{\hspace{2cm}}$ ,  $T = \underline{\hspace{2cm}}$ ,

b)  $p = \underline{\hspace{2cm}}$ ,  $T = \underline{\hspace{2cm}}$ ,

c)  $p = \underline{\hspace{2cm}}$ ,  $T = \underline{\hspace{2cm}}$ ,

d)  $p = \underline{\hspace{2cm}}$ ,  $T = \underline{\hspace{2cm}}$ .

Pretpostaviti da se smjesa vlada prema *Peng – Robinson* jednadžbi stanja. Kod proračuna primijeniti *pravila miješanja*.

### Mijenja se:

- Komponente
- Sastav
- Jednadžba stanja (RK, SRK, PR)
- Način izračunavanja parametara smjese (pravila miješanja, pseudokritični parametri)

# Plinske smjese

Redlich-Kwong jednačba stanja za smjesu:

$$p = \frac{RT}{v - b_M} - \frac{a_M}{\sqrt{T}v(v + b_M)}$$

**PRAVILA MIJEŠANJA**

Parametri jednačbe stanja za smjesu:

$$a_M = f(a_i)$$
$$b_M = f(b_i)$$

Parametri jednačbe stanja za komponente:

$$a_i = \frac{\Omega_a R^2 T_{K_i}^{5/2}}{p_K}$$
$$b_i = \frac{\Omega_b R T_{K_i}}{p_K}$$

Parametri jednačbe stanja za smjesu:

$$a_M = \frac{\Omega_a R^2 T_{KM}^{5/2}}{p_{KM}}$$
$$b_M = \frac{\Omega_b R T_{KM}}{p_{KM}}$$

Kritični parametri za smjesu:

$$T_{KM} = f(T_{K_i})$$
$$p_{KM} = f(p_{K_i})$$

**PSEUDOKRITIČNI PARAMETRI**

Ekperimentalni podaci: kritični parametri komponenta

$$p_{K_i}, T_{K_i}$$

# Plinske smjese

Pseudokritični parametri

Prausnitz-Gunn (1958)

$$v_{\text{KM}} = \sum y_i v_{\text{Ki}}$$

$$z_{\text{KM}} = \sum y_i z_{\text{Ki}}$$

$$T_{\text{KM}} = \sum y_i T_{\text{Ki}}$$

$$p_{\text{KM}} = \frac{z_{\text{KM}} RT_{\text{KM}}}{v_{\text{KM}}}$$

# Plinske smjese

Pravila miješanja

RK

$$b_M = \sum y_i b_i$$

$$B_M = \sum y_i B_i$$

$$a_M = \sum \sum y_i y_j a_{ij}$$

$$a_{ij} = \sqrt{a_i a_j}$$

$$A_M = \sum \sum y_i y_j A_{ij}$$

SRK, PR

$$b_M = \sum y_i b_i$$

$$B_M = \sum y_i B_i$$

$$(a\alpha)_M = \sum \sum y_i y_j (a\alpha)_{ij}$$

$$a_{ij} = (1 - k_{ij}) \sqrt{a_i a_j}$$

$$A_M = \sum \sum y_i y_j A_{ij}$$

# Umjesto zaključka

## Mrežne stranice FKIT-a

- I numericki seminar - priprema.pdf  
(Uvodni seminar za prvu vježbu – Powerpoint prezentacija)
- I numericki seminar - popis zadataka.pdf  
(Tekstovi zadataka)
- I numericki seminar - jednadzbe stanja.pdf  
(Tekst s potrebnim formulama i tablicama termodinamičkih svojstava)
- TRS Upute za pisanje referata.pdf  
(Upute za pisanje referata)
- I seminarski zadatak - popis studenata 2010.pdf  
(Popisi)

Potvrditi e-mailom prijam zadatka!

Želim Vam ugodan rad!