

# Osnove termodinamike realnih otopina

# Idealna otopina = ?

- Otopina – dvo- ili višekomponentni kondenzirani sustav
- Idealna otopina = stvar dogovora
- Idealno miješanje – proces nastajanja idealne otopine
- Usporedba termodinamičkih svojstava nastale otopine sa svojstvima komponenata
- Promatrat će se miješanje dviju kapljevina !!!!!!!!!!!

# Idealna otopina

Idealni volumen

$$V^{\text{id}} = V_1 + V_2$$

$$v^{\text{id}} = x_1 v_1 + x_2 v_2$$

Idealna entalpija

$$H^{\text{id}} = H_1 + H_2$$

$$h^{\text{id}} = x_1 h_1 + x_2 h_2$$

Gibbsova energija miješanja

(idealno miješanje je **spontan proces**)

$$G^{\text{id}} < G_1 + G_2$$

$$G^{\text{id}} = H^{\text{id}} - TS^{\text{id}}$$

$$S^{\text{id}} > 0$$

Idealna entropija

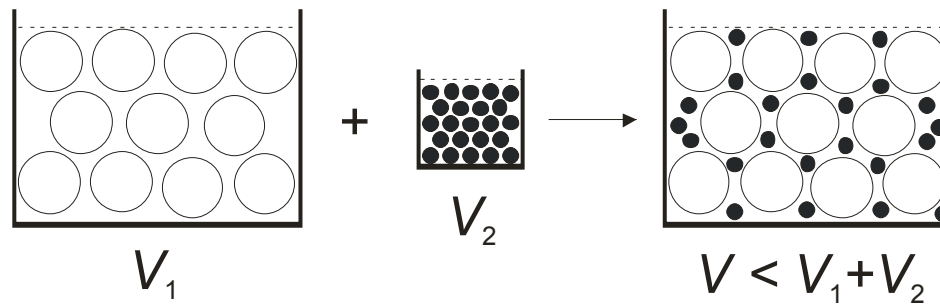
$$S^{\text{id}} = S_1 + S_2 - R(n_1 \ln x_1 + n_2 \ln x_2)$$

$$s^{\text{id}} = x_1 s_1 + x_2 s_2 - R(x_1 \ln x_1 + x_2 \ln x_2)$$

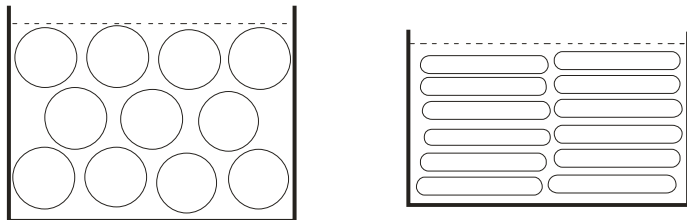
$$g^{\text{id}} = x_1 g_1 + x_2 g_2 + RT(x_1 \ln x_1 + x_2 \ln x_2)$$

# Uzroci neidealnosti volumena

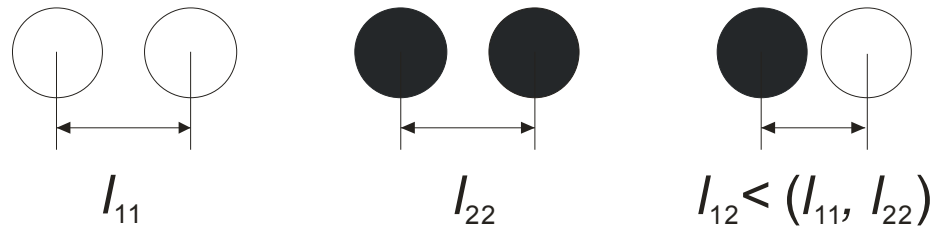
Razlika u veličini čestica



Razlika u obliku čestica

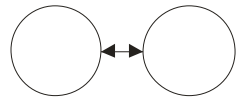


Međudjelovanja

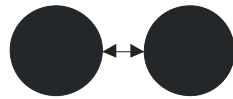


# Uzroci neidealnosti entalpije

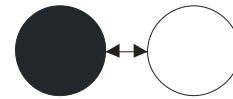
Međudjelovanja



$$\epsilon_{11}$$



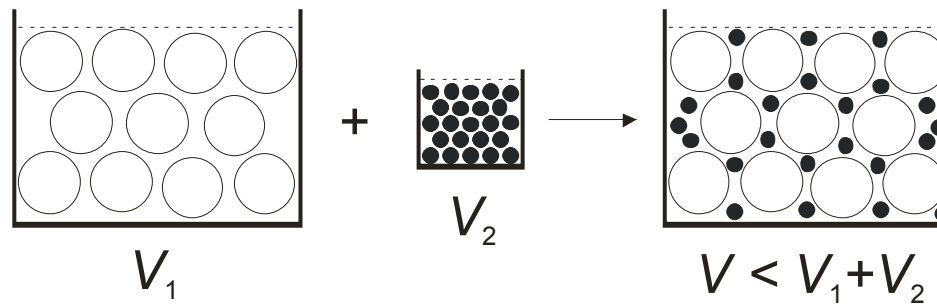
$$\epsilon_{22}$$



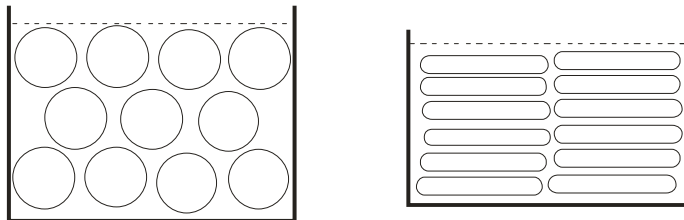
$$2\epsilon_{12} \neq \epsilon_{11} + \epsilon_{22}$$

# Uzroci neidealnosti entropije

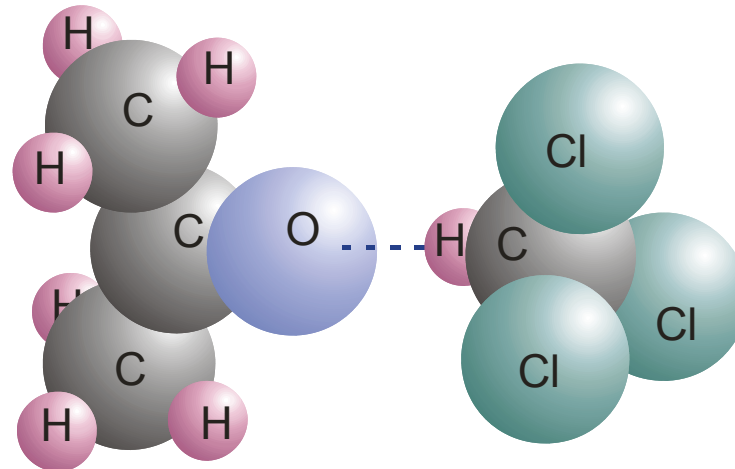
Razlika u veličini čestica



Razlika u obliku čestica



Međudjelovanja



# Idealno miješanje (zaključak)

- Proces nastajanja idealne otopine
- Idealna otopina nastaje miješanjem dviju komponenata čije su molekule **SLIČNE VELIČINE, SLIČNOGA OBLIKA I SLIČNIH MEĐUDJELOVANJA**
- **Slično se otapa u sličnome!**
- Radi se o otopinama (smjesama) **dviju kapljevina !!!!!!!!**

# Idealno miješanje (zaključak)

- Dogovorena definicija idealne otopine ne vrijedi za **asimetrične** sustave, tj. otopine plinova ili krutina u kapljevinama !!!

$$v^{\text{id}} = x_1 v_1^{\text{L}} + x_2 v_2^{\text{L}}$$

$$h^{\text{id}} = x_1 h_1^{\text{L}} + x_2 h_2^{\text{L}}$$

$$s^{\text{id}} = x_1 s_1^{\text{L}} + x_2 s_2^{\text{L}} - R(x_1 \ln x_1 + x_2 \ln x_2)$$

ZAŠTO ?

- Što s nesimetričnim sustavima? Koja je definicija idealne otopine za npr. otopine plinova u kapljevinama ili otopine krutina u kapljevinama?



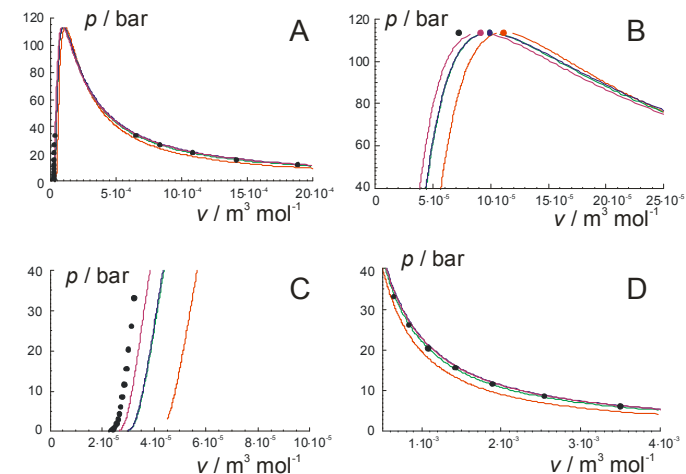
# Opis otopina jednadžbama stanja

Mogu li se termodinamičke veličine kapljevina izračunati jednadžbama stanja ?

$$v^3 - v^2 \left( b + \frac{RT}{p} \right) + v \left( \frac{a}{p} \right) - \frac{ab}{p} = 0$$

$$h = h_{\text{ref}} + \int_{T^\circ}^T c_p^{\text{id}} dT + RT(z-1) + \int_{\infty}^v \left[ T \left( \frac{\partial p}{\partial T} \right)_v - p \right] dv$$

$$s = s_{\text{ref}} + \int_{T^\circ}^T \frac{c_p^{\text{id}}}{T} dT + R \ln \frac{v}{v^\circ} + \int_{\infty}^v \left[ \left( \frac{\partial p}{\partial T} \right)_v - \frac{R}{v} \right] dv$$



Ima li to uopće smisla ?

# Opis otopina jednadžbama stanja

Mogu li se termodinamičke veličine kapljevine izračunati jednadžbama stanja ?



Ima li to uopće smisla ?

# Veličine miješanja

$$V^M = V - (V_1 + V_2)$$

$$v^M = v - (x_1 v_1 + x_2 v_2)$$

$$S^M = S - (S_1 + S_2)$$

$$s^M = s - (x_1 s_1 + x_2 s_2)$$

$$H^M = H - (H_1 + H_2)$$

$$h^M = h - (x_1 h_1 + x_2 h_2)$$

$$G^M = G - (G_1 + G_2)$$

$$g^M = g - (x_1 g_1 + x_2 g_2)$$

$$Y^M = Y - (Y_1 + Y_2)$$

$$y^M = y - (x_1 y_1 + x_2 y_2)$$

$$y^M = y - \sum x_i y_i$$

Veličine miješanja određuju se eksperimentom !

Stanje nakon miješanja minus stanje prije miješanja

# Veličine miješanja pri idealnom miješanju

$$V^M = V - (V_1 + V_2)$$

$$V^{M,\text{id}} = (V_1 + V_2) - (V_1 + V_2) = 0$$

$$v^{M,\text{id}} = 0$$

$$H^M = H - (H_1 + H_2)$$

$$H^{M,\text{id}} = (H_1 + H_2) - (H_1 + H_2) = 0$$

$$h^{M,\text{id}} = 0$$

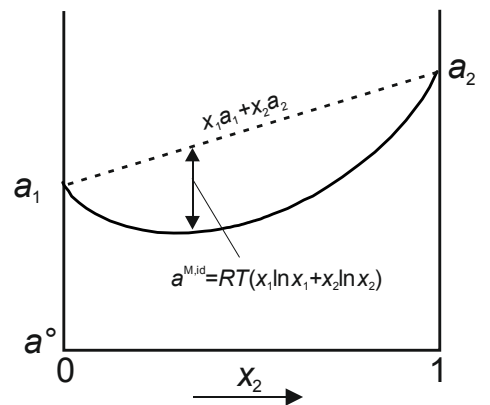
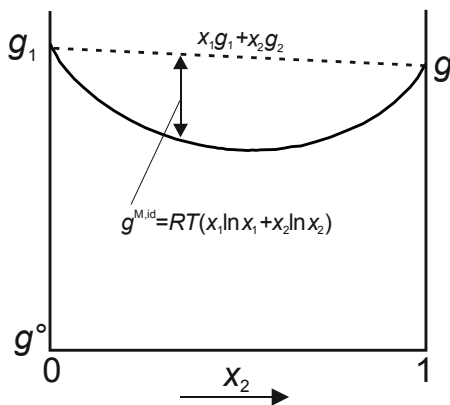
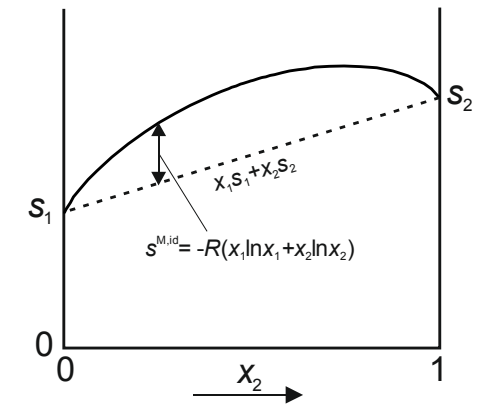
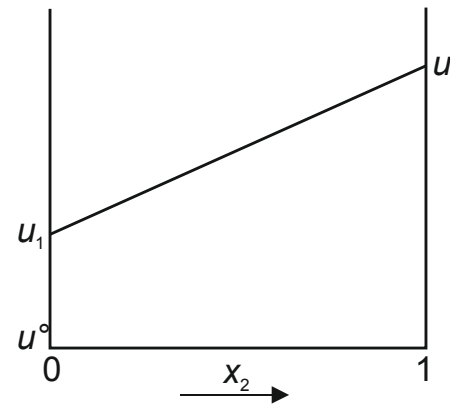
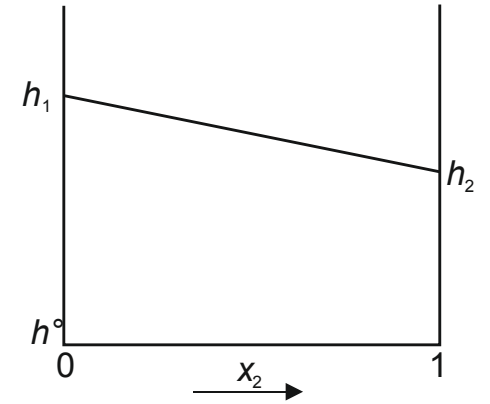
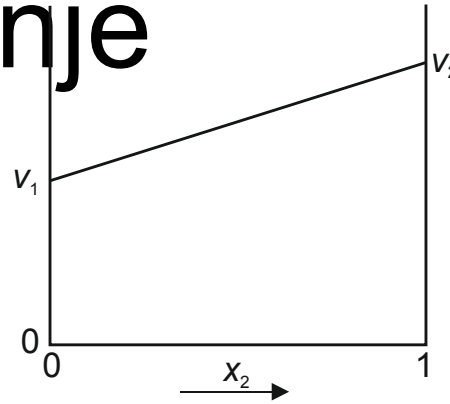
$$S^M = S - (S_1 + S_2)$$

$$S^{M,\text{id}} = [S_1 + S_2 - R(n_1 \ln x_1 + n_2 \ln x_2)] - (S_1 + S_2) = -R(n_1 \ln x_1 + n_2 \ln x_2)$$

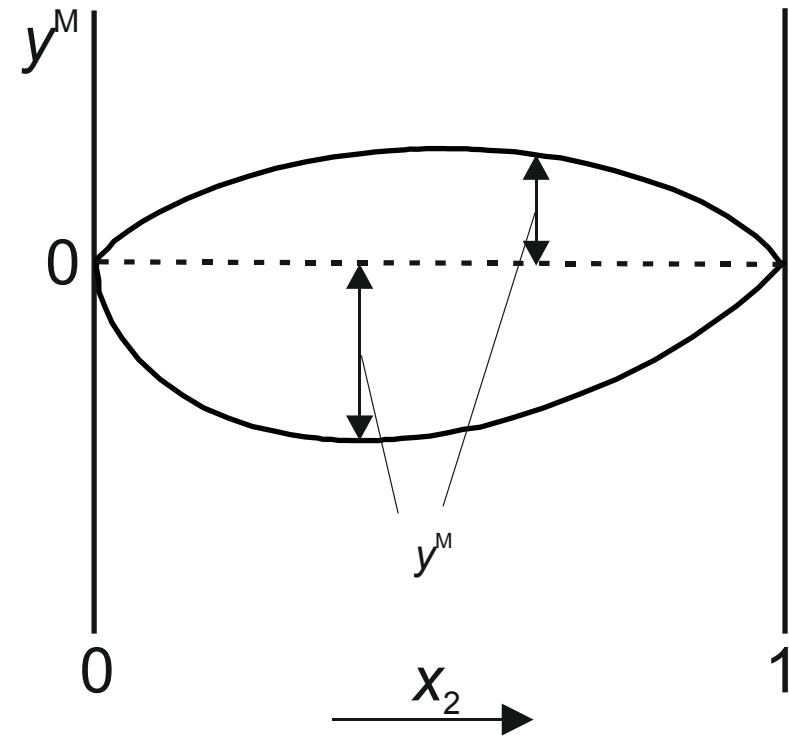
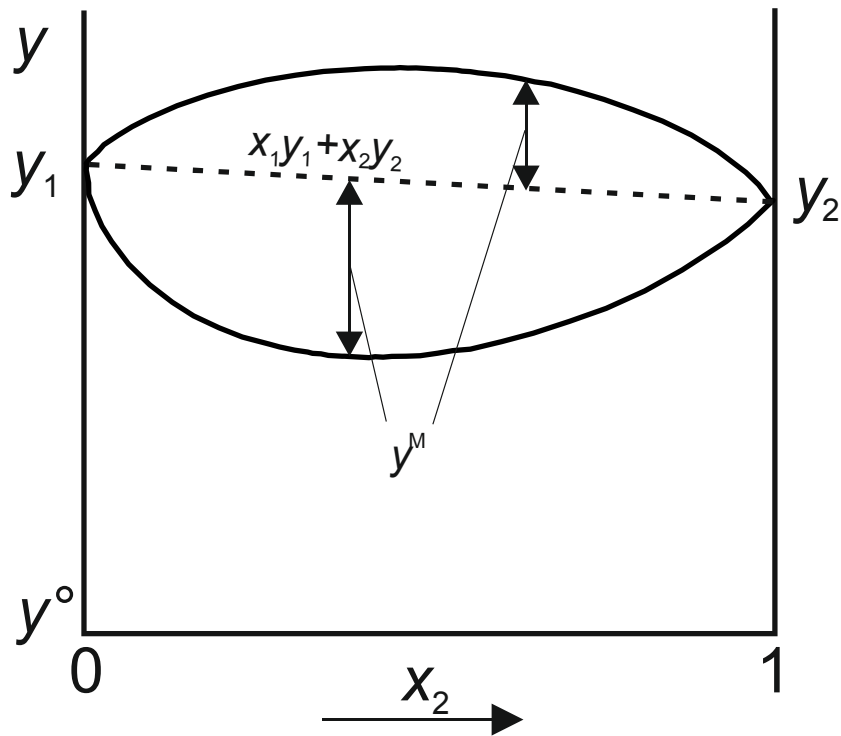
$$s^{M,\text{id}} = -R \sum x_i \ln x_i$$

# Idealno miješanje (zaključak)

Veličina	Iznos promjene
$V_M^{\text{id}}$	0
$u_M^{\text{id}}$	0
$h_M^{\text{id}}$	0
$s_M^{\text{id}}$	$-R \sum x_i \ln x_i$
$g_M^{\text{id}}$	$RT \sum x_i \ln x_i$
$a_M^{\text{id}}$	$RT \sum x_i \ln x_i$



# Veličine miješanja pri realnom miješanju



# Ekscesne veličine

$$V^{\text{ex}} = V - V^{\text{id}} \quad H^{\text{ex}} = H - H^{\text{id}} \quad S^{\text{ex}} = S - S^{\text{id}}$$

$$v^{\text{ex}} = v - v^{\text{id}} \quad h^{\text{ex}} = h - h^{\text{id}} \quad s^{\text{ex}} = s - s^{\text{id}}$$

$$Y^{\text{ex}} = Y - Y^{\text{id}}$$

$$y^{\text{ex}} = y - y^{\text{id}}$$

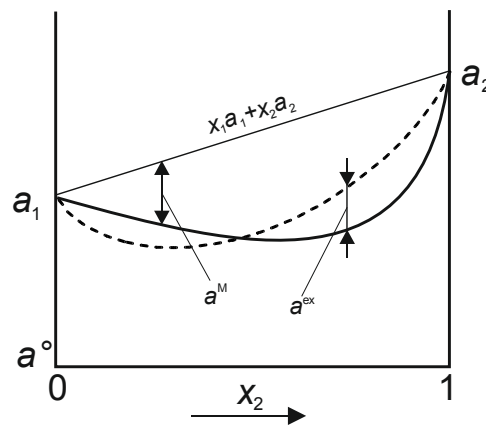
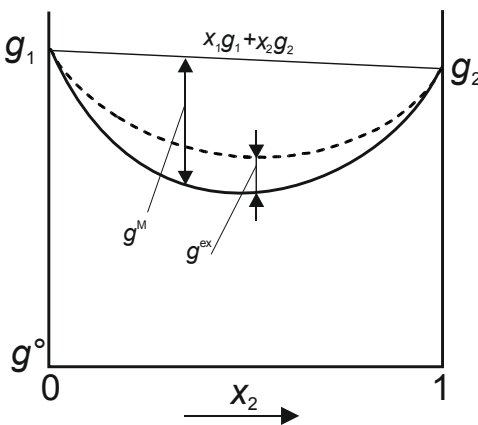
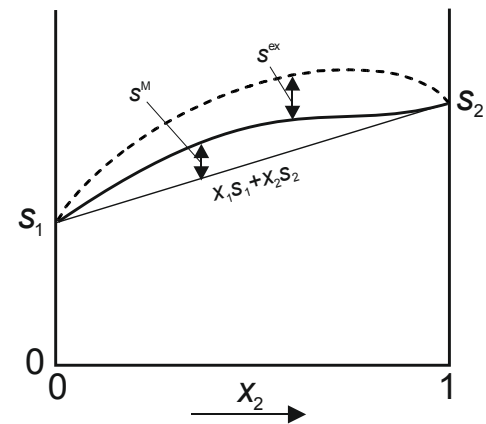
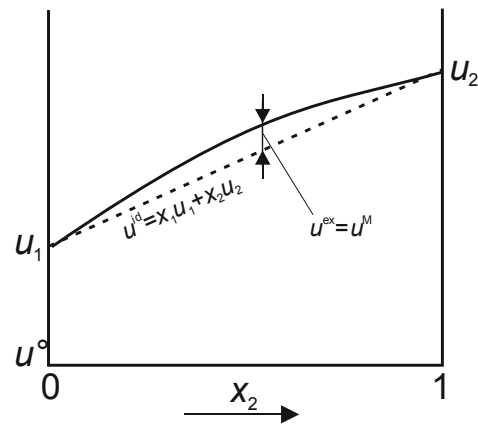
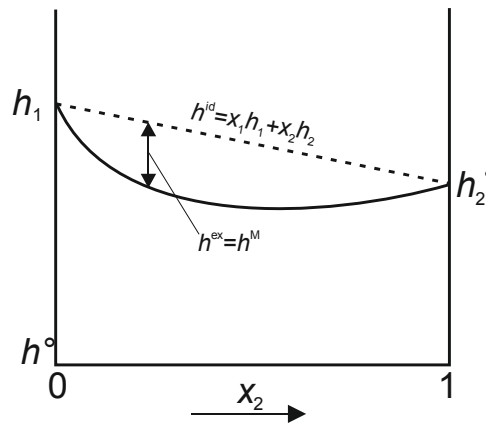
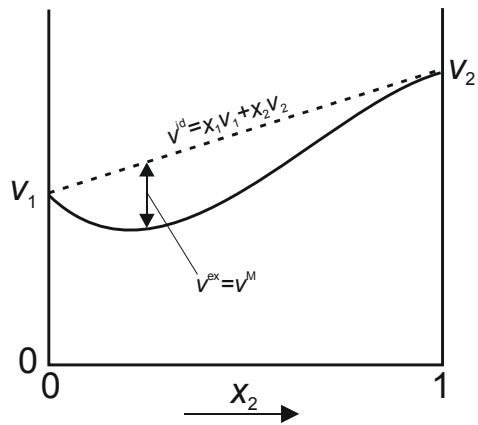
Iznos ekscesnih veličina ovisi o izboru idealne otopine !

Radi se o razlici mjerene (mjerljive) veličine i zamišljene (dogovorene veličine)

Stanje nakon realnog miješanja minus stanje nakon (zamišljenog) idealnog miješanja

# Ekscesne veličine

Uz dogovorenu definiciju idealne otopine



$$v^{ex} = v^M$$

$$h^{ex} = h^M$$

$$u^{ex} = u^M$$

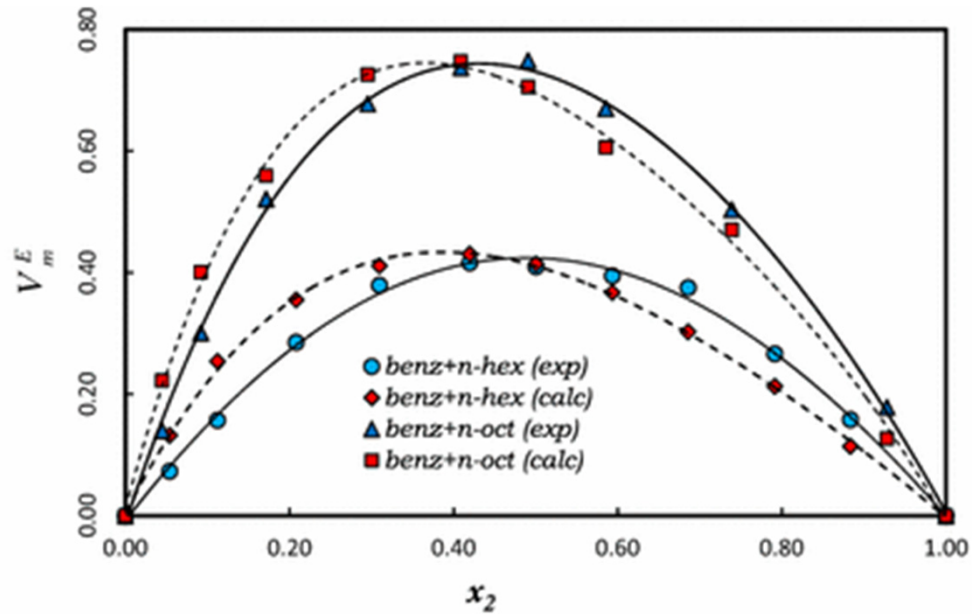
$$s^{ex} \neq s^M$$

$$g^{ex} \neq g^M$$

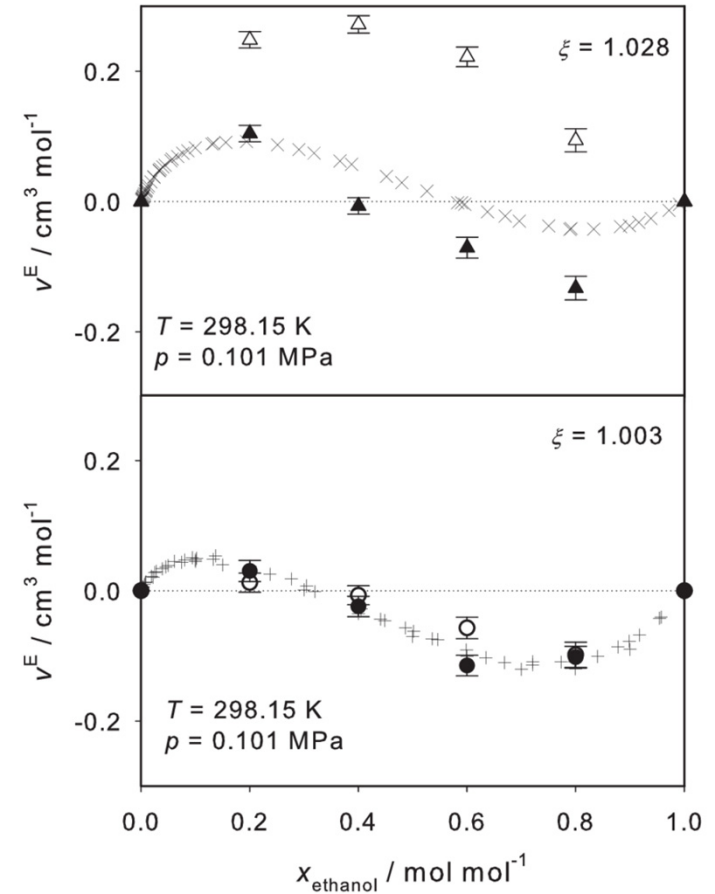
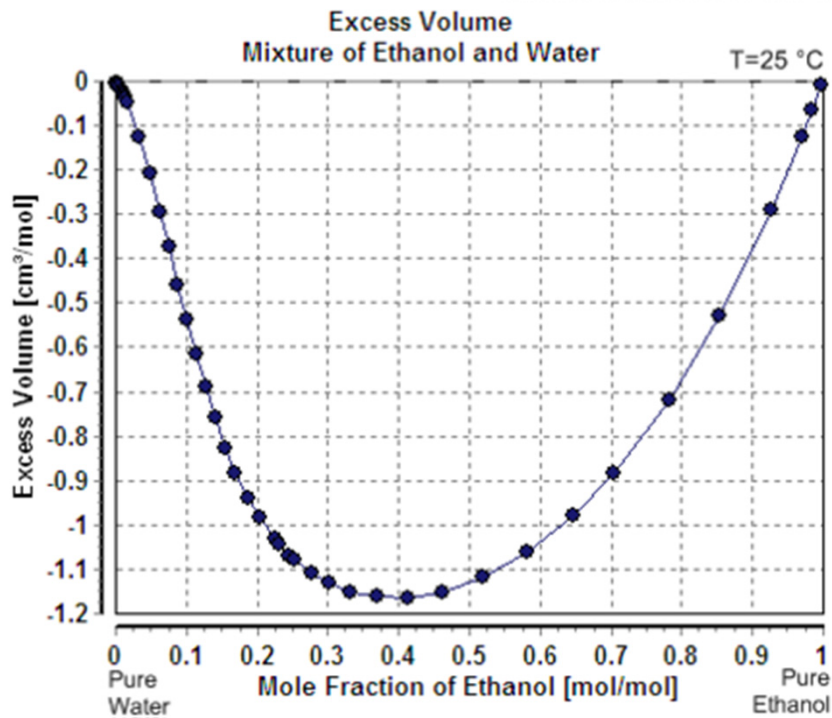
$$a^{ex} \neq a^M$$



# Ekscesne veličine

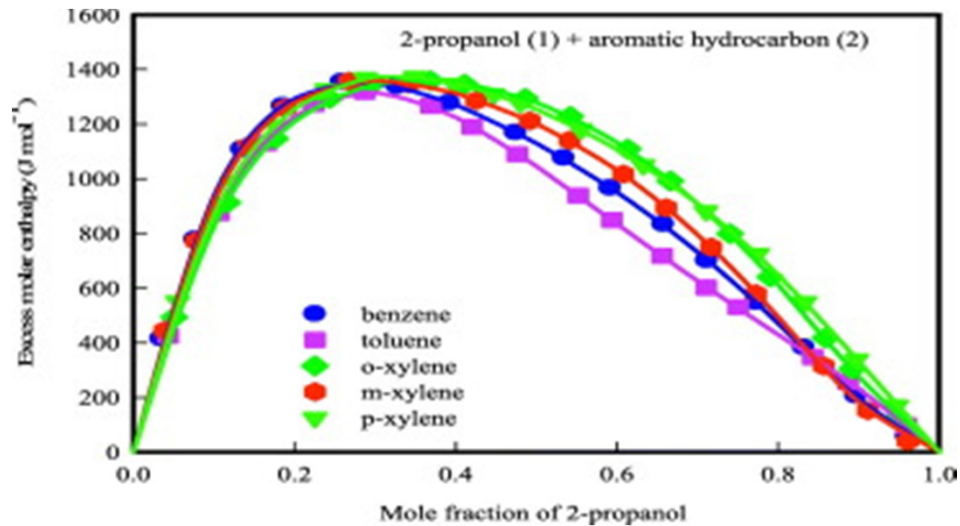
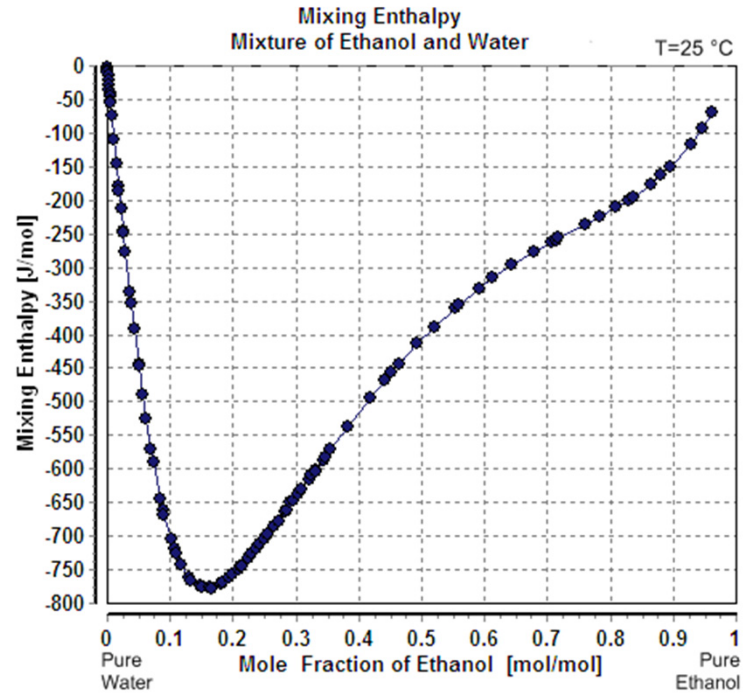


Data taken from Dortmund Data Bank

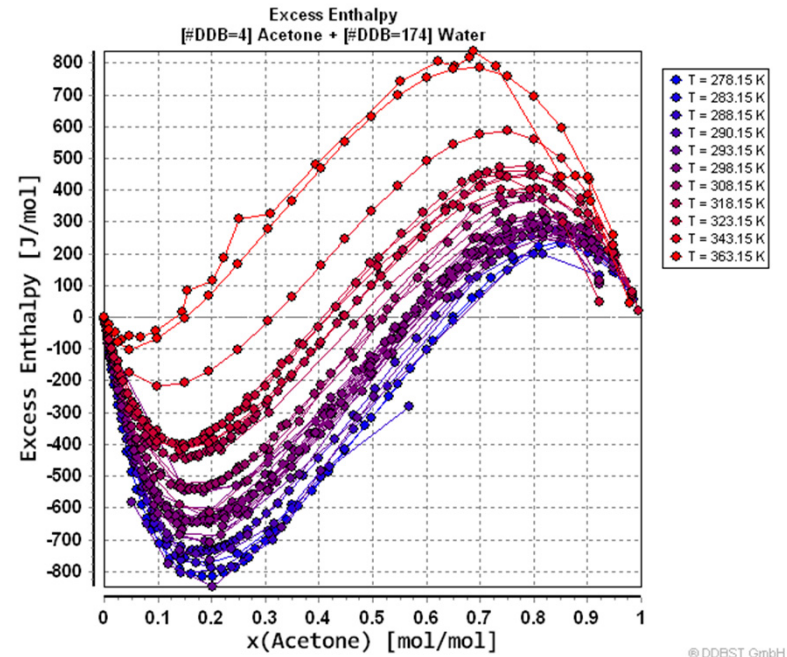


Etanol – benzen  
Etanol – toluen

Data taken from Dortmund Data Bank

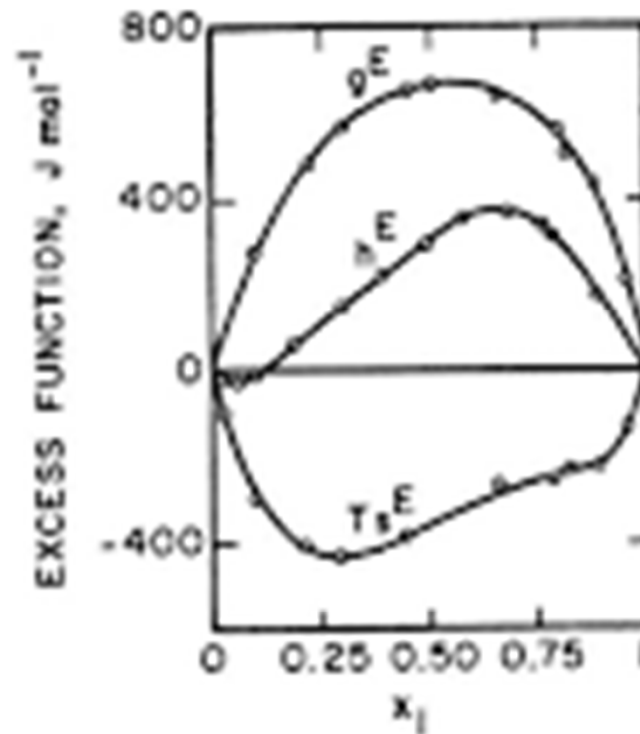


# Ekscesne veličine



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# Ekscesne veliĉine



**Figure 6-8** Excess functions for the acetic acid (1)/water (2) system at 25°C (R. Haase *et al.*, 1973, *Z. Naturforschung*, 28a: 1740).

# Parcijalne molarne veličine

Formalno značenje

$$V = f(p, T, n_1, n_2)$$

$$dV = \left( \frac{\partial V}{\partial p} \right)_{T, n_1, n_2} dp + \left( \frac{\partial V}{\partial T} \right)_{p, n_1, n_2} dT + \left( \frac{\partial V}{\partial n_1} \right)_{p, T, n_2} dn_1 + \left( \frac{\partial V}{\partial n_2} \right)_{p, T, n_1} dn_2$$

$$dV = \left( \frac{\partial V}{\partial n_1} \right)_{p, T, n_2} dn_1 + \left( \frac{\partial V}{\partial n_2} \right)_{p, T, n_1} dn_2$$

$$\bar{v}_1 = \left( \frac{\partial V}{\partial n_1} \right)_{p, T, n_2}$$

$$\bar{v}_2 = \left( \frac{\partial V}{\partial n_2} \right)_{p, T, n_1}$$

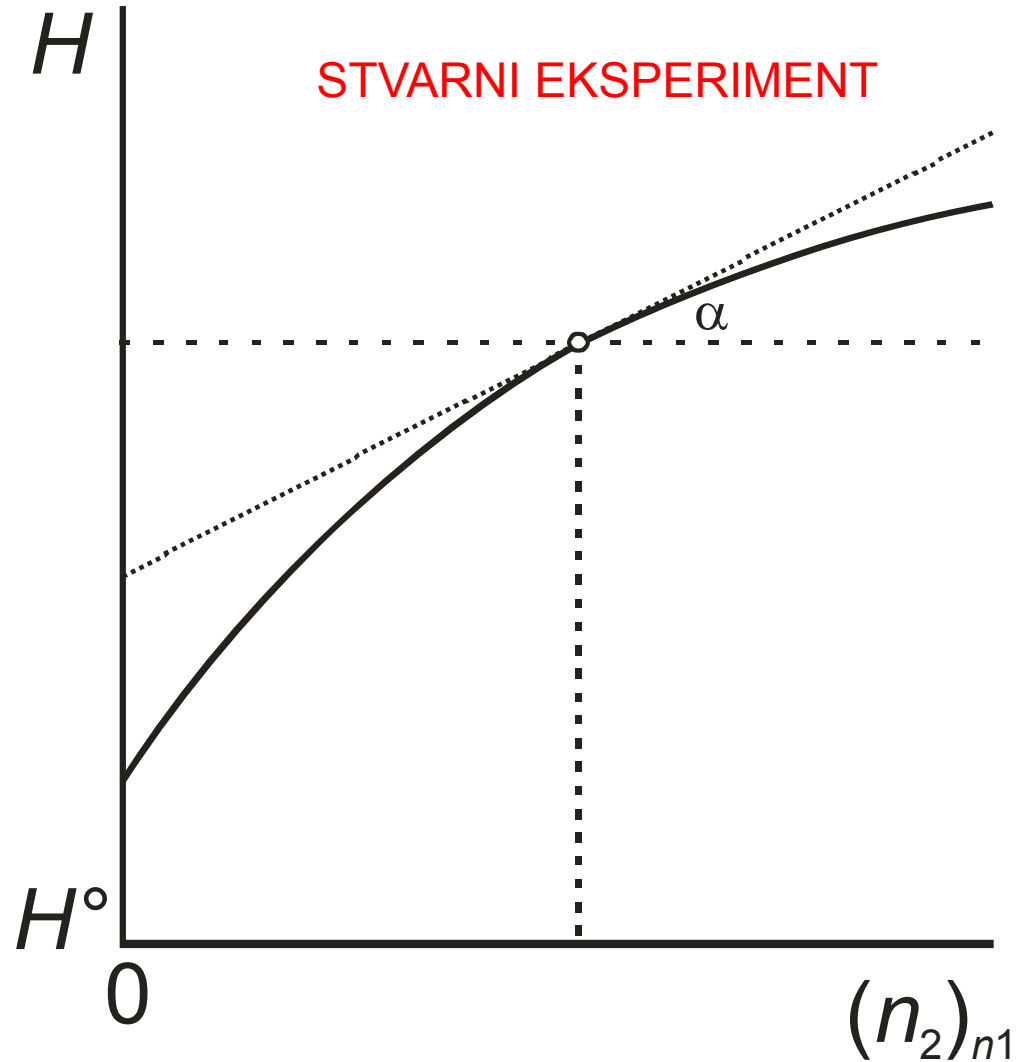


# Određivanje PMV – 1

Metoda tangente

$$\bar{h}_1 = \left( \frac{\partial H}{\partial n_1} \right)_{p, T, n_{j \neq i}}$$

$$\bar{h}_2 = \left( \frac{\partial H}{\partial n_2} \right)_{p, T, n_1}$$



# Parcijalne molarne veličine

Idealne otopine

$$V^{\text{id}} = n_1 v_1 + n_2 v_2$$

$$v^{\text{id}} = x_1 v_1 + x_2 v_2$$

Realne otopine

Formalna analogija

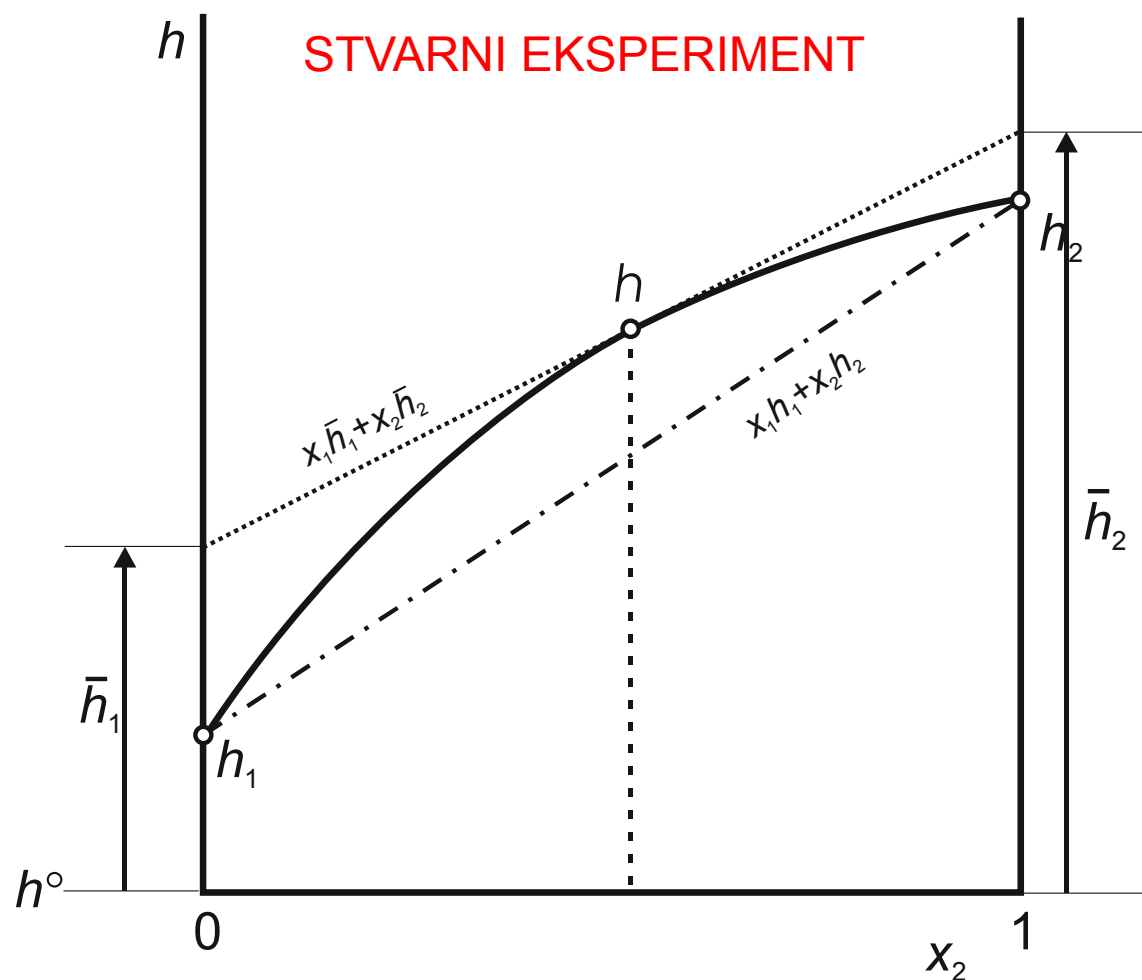
$$V = n_1 \bar{v}_1 + n_2 \bar{v}_2$$

$$v = x_1 \bar{v}_1 + x_2 \bar{v}_2$$

Koliki dio realne otopine „otpada” na pojedinu komponentu

# Određivanje PMV – 2

Metoda odsječka (intercepta)



$$h = x_1 \bar{h}_1 + x_2 \bar{h}_2$$

$$x_1 = 1 - x_2$$

$$h = \bar{h}_1 + x_2 (\bar{h}_2 - \bar{h}_1)$$

# Parcijalne molarne veličine

$$\bar{y}_i = \left( \frac{\partial Y}{\partial n_i} \right)_{p, T, n_{j \neq i}}$$

$$Y = \sum n_i \bar{y}_i$$

$$y = \sum x_i \bar{y}_i$$

$$\bar{y}_i = y - \sum_{k \neq i} x_k \left( \frac{\partial y}{\partial x_k} \right)_{p, T, x_{j \neq i, k}}$$

$$\bar{h}_i = \bar{u}_i + p \bar{v}_i$$

$$\bar{g}_i = \bar{h}_i - T \bar{s}_i$$

$$\frac{\partial(\bar{g}_i/T)}{\partial T} = -\frac{\bar{h}_i}{T^2}$$

$$\left( \frac{\partial \bar{h}_i}{\partial T} \right)_p = \bar{c}_{p, i}$$



# Parcijalne molarne veličine miješanja i parcijalne molarne ekscesne veličine

$$V^M = V - (V_1 + V_2)$$

$$V^{\text{ex}} = V - V^{\text{id}}$$

$$v^M = v - (x_1 v_1 + x_2 v_2)$$

$$v^{\text{ex}} = v - (x_1 v_1 + x_2 v_2)$$

$$v^M = x_1 \bar{v}_1 + x_2 \bar{v}_2 - (x_1 v_1 + x_2 v_2)$$

$$v^{\text{ex}} = x_1 \bar{v}_1 + x_2 \bar{v}_2 - (x_1 v_1 + x_2 v_2)$$

$$Y^M = \sum n_i (\bar{y}_i - y_i)$$

$$y^M = \sum x_i (\bar{y}_i - y_i)$$

Parcijalne molarne veličine miješanja

$$y^M = \sum x_i \bar{y}_i^M$$

$$\bar{y}_i^M = \bar{y}_i - y_i$$

Parcijalne molarne ekscesne veličine

$$y^{\text{ex}} = \sum x_i \bar{y}_i^{\text{ex}} \quad \bar{v}_i^{\text{ex}} = \bar{v}_i - v_i = \bar{v}_i^M$$

$$\bar{a}_i^{\text{ex}} = \bar{a}_i - a_i - RT \ln x_i \neq \bar{a}_i^M$$

# Gibbs-Duhemova rovnice

Totalní diferenciál

$$dV = n_1 d\bar{v}_1 + n_2 d\bar{v}_2 + \bar{v}_1 dn_1 + \bar{v}_2 dn_2$$

Definice

$$dV = \bar{v}_1 dn_1 + \bar{v}_2 dn_2$$

Gibbs-Duhem

$$n_1 d\bar{v}_1 + n_2 d\bar{v}_2 = 0$$

$$x_1 d\bar{v}_1 + x_2 d\bar{v}_2 = 0$$

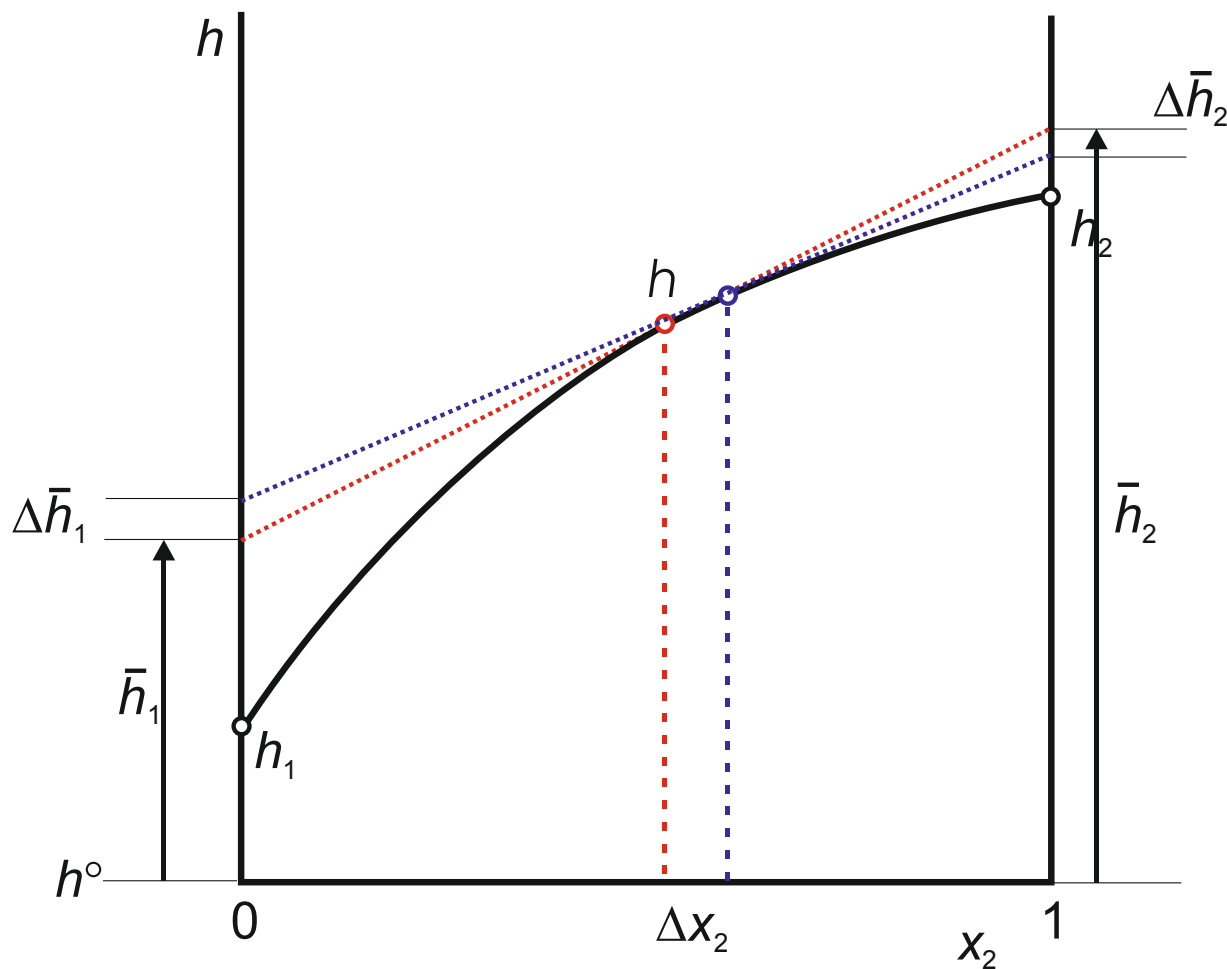
Višekomponentní systémy

$$\sum n_i d\bar{y}_i = 0$$

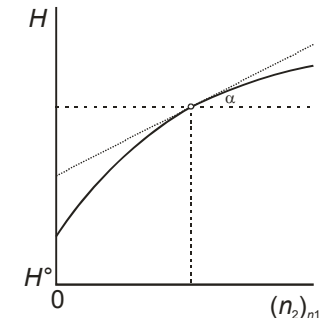
$$\sum x_i d\bar{y}_i = 0$$

# Gibbs-Duhemova jednadžba

Međuviznost parcijalnih molarnih veličina



Primjena



$$x_1 d\bar{h}_1 + x_2 d\bar{h}_2 = 0$$

$$d\bar{h}_1 = -\frac{x_2}{x_1} d\bar{h}_2$$

$$\lim_{x_1 \rightarrow 1} \bar{h}_1 = h_1$$

$$\bar{h}_1 = h_1 - \int_{\bar{h}_2(x_2=0)}^{\bar{h}_2} \frac{x_2}{x_1} d\bar{h}_2$$

# Aktivnost i standardna stanja

- Što je aktivnost čistih plinova ?
- Kako mjeriti aktivnost molekula u čistim plinovima ?
- **Prirodna mjera aktivnosti ?**

## IDEALNI PLINOVI

$$(dg)_T = RTd \ln p$$

## REALNI PLINOVI

Fugacitivnost  $(dg)_T = RTd \ln f$

## Standardno stanje

$$g = g^\circ + RT \ln \frac{p}{p^\circ} \quad a = \frac{p}{p^\circ}$$

$$g = g^\circ + RT \ln \frac{f}{f^\circ} \quad a = \frac{f}{f^\circ} \quad \text{Lewis}$$

Standardno stanje – stanje čistog plina pri temperaturi  $T$  i referentnom tlaku  $p^\circ$  (1 bar)

Definicija se upotpunjuje odgovarajućim iznosom entalpije

# Parcijalne fugacitivnosti

## Idealna plinska smjesa

Smjesa dvaju ili više plinova koja ne mora biti idealni plin, ali jest idealna otopina, sukladno dogovorenoj definiciji idealne otopine

$$v^{M,id} = 0$$

$$h^{M,id} = 0$$

$$s^{M,id} = -R \sum y_i \ln y_i$$

Za čisti plin fugacitivnost se uspoređuje s tlakom:

$$\ln \frac{f}{p} = \frac{(g - g^\circ)}{RT} = \frac{1}{RT} \int_0^p \left( v - \frac{RT}{p} \right) dp$$

$$\bar{v}_i = v_i$$

Za plinsku smjesu parcijalna fugacitivnost uspoređuje se s parcijalnim tlakom:

$$\ln \frac{\hat{f}_i}{p_i} = \frac{(\bar{g}_i - \bar{g}_i^{id})}{RT} = \frac{1}{RT} \int_0^{p_i} (\bar{v}_i - \bar{v}_i^{id}) dp$$

Parcijalni koeficijent fugacitivnosti

$$\hat{\phi}_i = \frac{\hat{f}_i}{y_i p}$$

$$\ln \frac{\hat{f}_i}{y_i p} = \frac{(\bar{g}_i - \bar{g}_i^{id})}{RT} = \frac{1}{RT} \int_0^{p_i} \left( \bar{v}_i - \frac{RT}{p} \right) dp$$

# Aktivnost i standardna stanja

- Što je aktivnost komponente u plinskoj smjesi ?
- Kako mjeriti aktivnost molekula komponenata u plinskim smjesama ? **Elektrodni potencijal ?**
- **Prirodna mjera aktivnosti ?**

## IDEALNE PLINSKE SMJESE

$$(d\bar{g}_i)_T = RTd \ln p_i$$

$$(d\mu_i)_T = RTd \ln p_i$$

$$\mu_i = \mu_i^\circ + RT \ln \frac{p_i}{p^\circ} \quad a_i = \frac{p_i}{p^\circ}$$

## KEMIJSKI POTENCIJAL

## REALNE PLINSKE SMJESE

Parcijalna  
fugacitivnost

$$(d\bar{g}_i)_T = RTd \ln \hat{f}_i$$

$$(d\mu_i)_T = RTd \ln \hat{f}_i$$

$$\mu_i = \mu_i^\circ + RT \ln \frac{\hat{f}_i}{f^\circ} \quad a_i = \frac{\hat{f}_i}{f^\circ} \quad \text{Lewis}$$

Standardno stanje – stanje čistog plina pri temperaturi  $T$   
i referentnom tlaku  $p^\circ$  (1 bar)

Definicija se upotpunjuje odgovarajućim iznosom entalpije

Standardno stanje

# Aktivnost i standardna stanja

Čiste kapljevine i krutine

- Aktivnost čistih kapljevina i krutina po definiciji iznosi 1
- jer se kao **standardno stanje** odabire stanje čiste kapljevine, odnosno krutine pri temperaturi  $T$  i tlaku sustava  $p$

$$g = g^\circ + RT \ln \frac{f}{f^\circ}$$

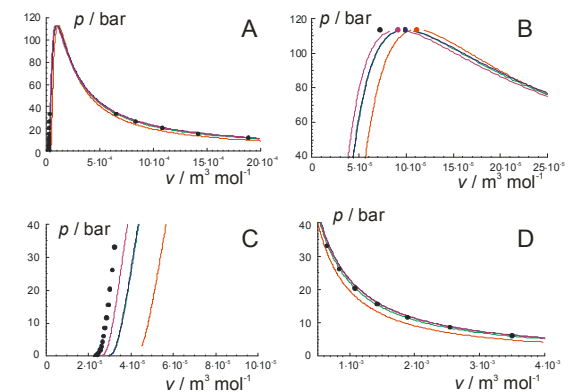
Fugacitivnost pri temperaturi i tlaku sustava)

Fugacitivnost u standardnom stanju (pri temperaturi i tlaku sustava)

$$a = \frac{f}{f^\circ} \quad a = 1$$

Kolika je fugacitivnost čiste kapljevine, odnosno krutine (kapljevine, odnosno krutine u standardnom stanju) ?

$$\ln \varphi = \ln \frac{v}{v-b} + \frac{a\alpha(T)}{bRT} \ln \frac{v}{v+b} + (z-1) - \ln z$$



# Fugacitivnost čiste kapljevine ili krutine

- Vrijednosti fugacitivnosti kapljevine (krutine) moraju biti konzistentne s onima u plinskoj fazi
- Fugacitivnost plina računa se jednadžbom stanja
- Fugacitivnost kapljevine (krutine) računa se iz eksperimentalnog podatka o gustoći kapljevine (krutine)

$$g^L = g^V$$

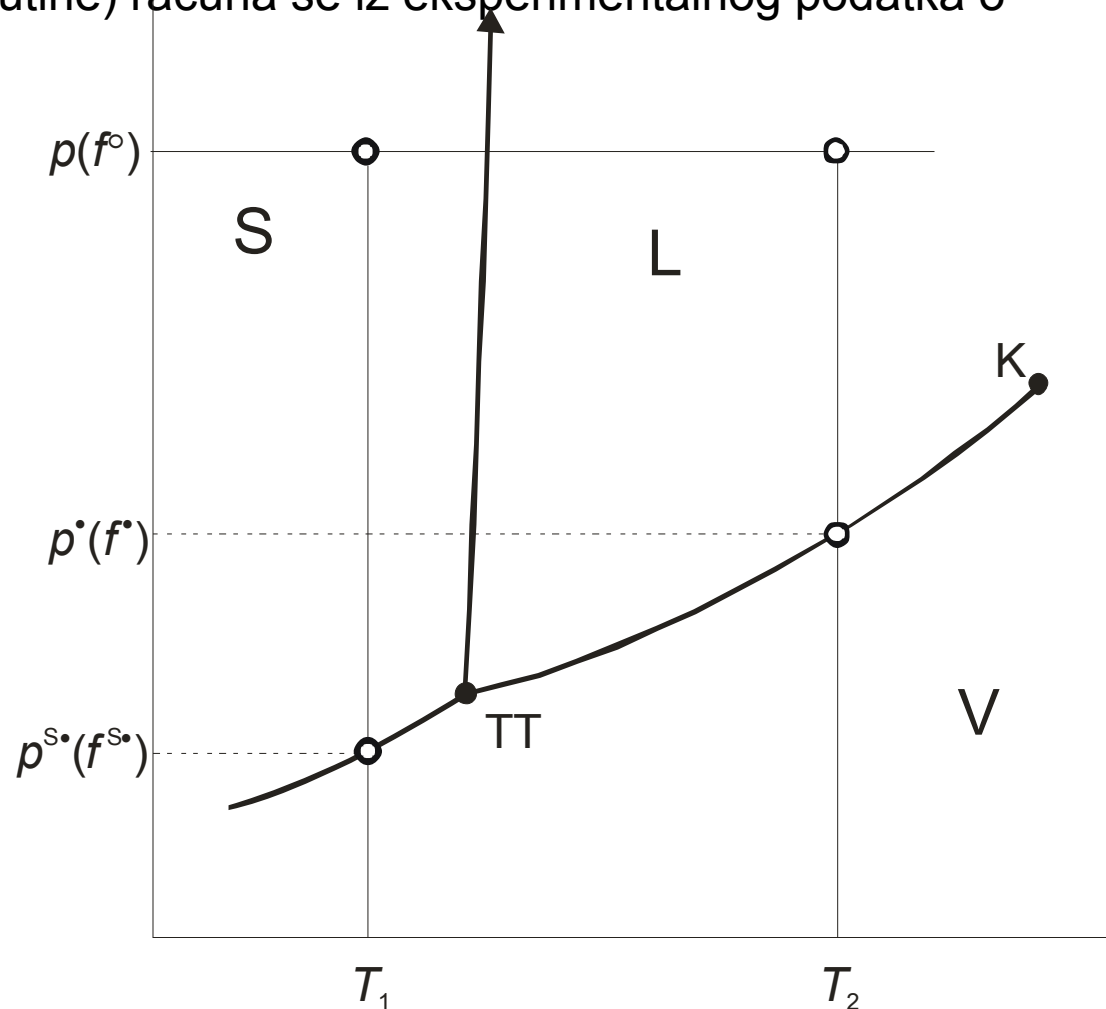
$$f^L = f^V = f^\bullet$$

$$RT d \ln f = v^L dp$$

$$\int_{f^\bullet}^{f^\circ} d \ln f = \frac{1}{RT} \int_{p^\bullet}^p v^L dp$$

$$f^\circ = f^\bullet \exp \left( \frac{1}{RT} \int_{p^\bullet}^p v^L dp \right)$$

$$f^\bullet = \varphi^\bullet p^\bullet \quad v^L = \frac{M}{\rho}$$





# Fugacitivnost čiste kapljevine ili krutine

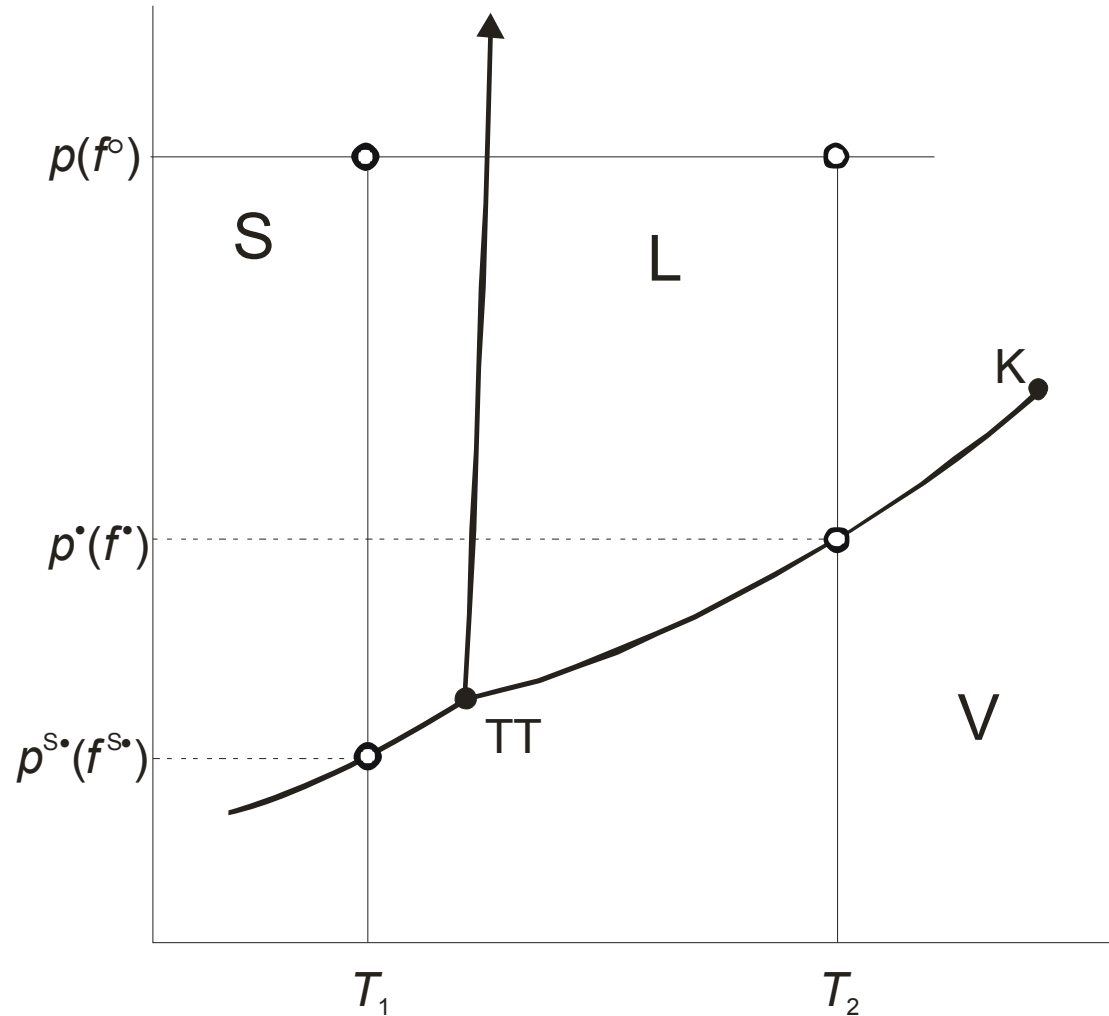
Poyntingov faktor

$$PF = \exp \left[ \frac{v^L (p - p^\bullet)}{RT} \right]$$

Krutina

$$f^\circ = f^{S^\bullet} \exp \left( \frac{1}{RT} \int_{p^{S^\bullet}}^p v^S dp \right) =$$

$$= \varphi^{S^\bullet} p^{S^\bullet} \exp \left[ \frac{v^S (p - p^{S^\bullet})}{RT} \right]$$



# Aktivnost i standardna stanja

## Smjese kapljevina (otopine)

- Što je aktivnost komponente u kapljevitoj smjesi ?
- Kako mjeriti aktivnost molekula komponenata u kapljevitim smjesama ? Elektrodni potencijal ? Osmotski tlak? Povišenje vrelišta ? Sniženje ledišta ? Tlak para ?
- U idealnim otopinama u jednadžbe ide množinski udio komponente, u realnima aktivnost komponente !!!!
- Aktivnost komponente u otopini stoga je manje-više izravno povezana s njenim množinskim udjelom → za čistu tvar aktivnost je 1, a kad komponente nema u sustavu aktivnost je 0 !!!

# Aktivnost i standardna stanja

## Smjese kapljevina (otopine)

- Formalne jednadžbe su slične kao i za smjese plinova !!!

$$\mu_i = \mu_i^\circ + RT \ln \frac{p_i}{p^\circ} \quad a_i = \frac{p_i}{p^\circ} \quad \mu_i = \mu_i^\circ + RT \ln \frac{\hat{f}_i}{f_i^\circ} \quad a_i = \frac{\hat{f}_i}{f_i^\circ}$$

Veza aktivnosti i množinskog udjela je “racionalni” koeficijent aktivnosti

$$\gamma_i = \frac{a_i}{x_i} \quad \hat{f}_i = \gamma_i x_i f_i^\circ$$

$\gamma_i > 1$  znači da je aktivnost veća od množinskog udjela →  
mjereno svojstvo ukazuje na to da mu komponenta više pridonosi od  
očekivanoga sukladno sastavu otopine

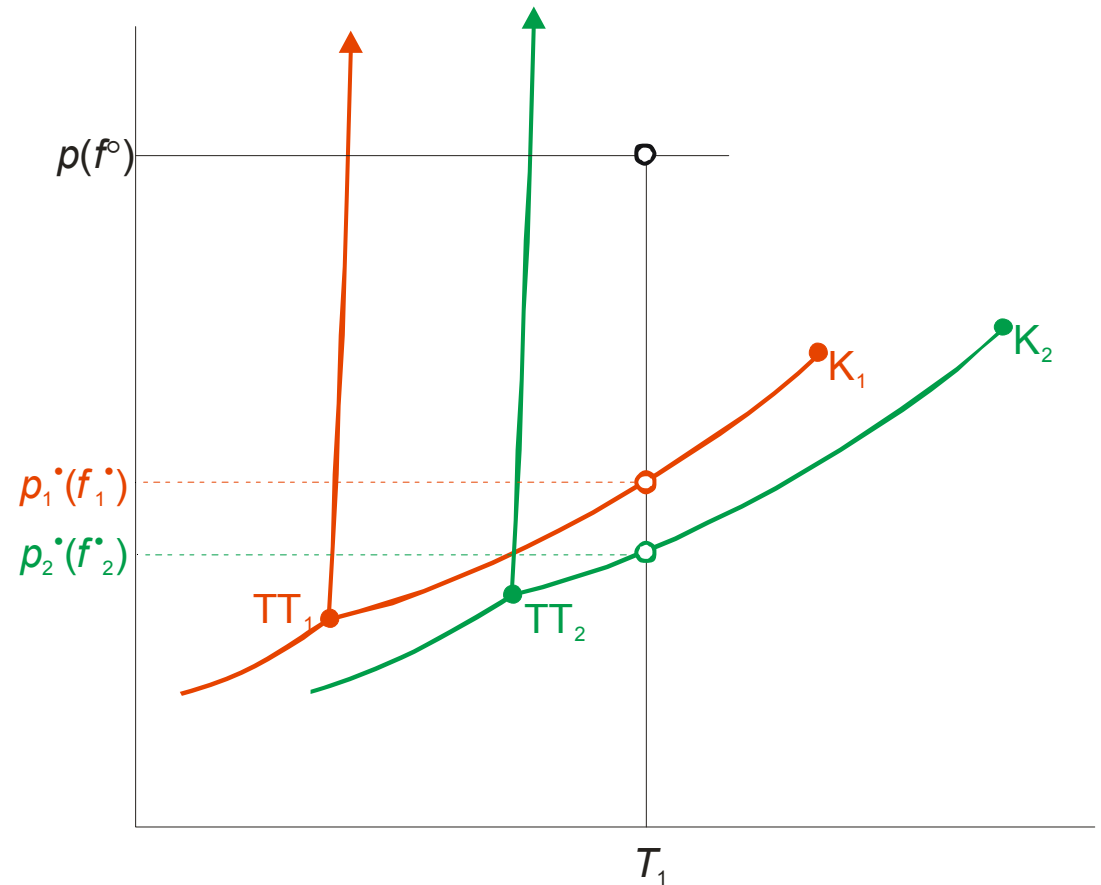
Za idealne otopine ili idealne plinske smjese:  
Vrijedi tzv. Lewis-Randallovo pravilo

$$\gamma_i = 1 \quad \hat{f}_i = x_i f_i^\circ \quad v^M = 0$$
$$\hat{f}_i = y_i f_i^\circ \quad \hat{\phi}_i = \phi_i^\circ$$

# Standardne fugacitivnosti komponenata u otopinama (smjesama) dviju kapljevina

Standardno stanje – čista kapljevina pri temperaturi i tlaku sustava

$$f_i^\circ = f_i^\bullet \exp\left(\frac{1}{RT} \int_{p_i^\bullet}^p v_i^L dp\right)$$



# Aktivnosti komponenata u otopinama (smjesama) dviju kapljevina

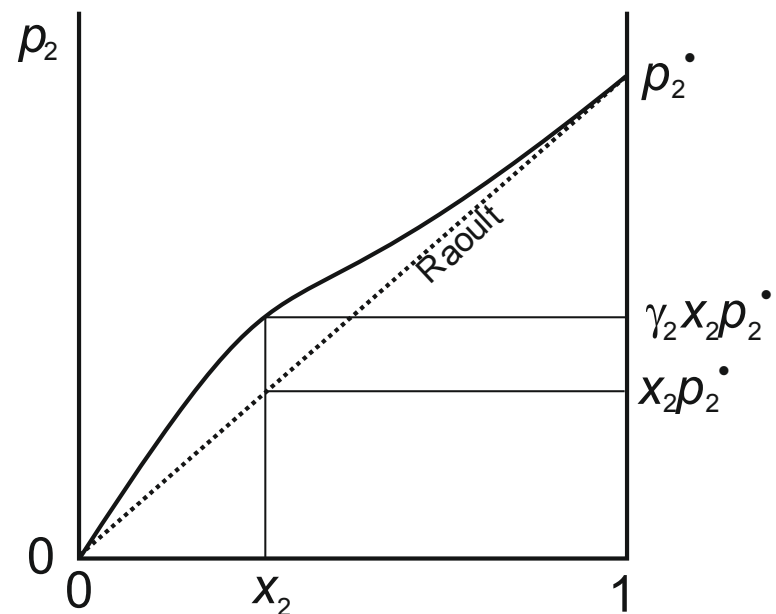
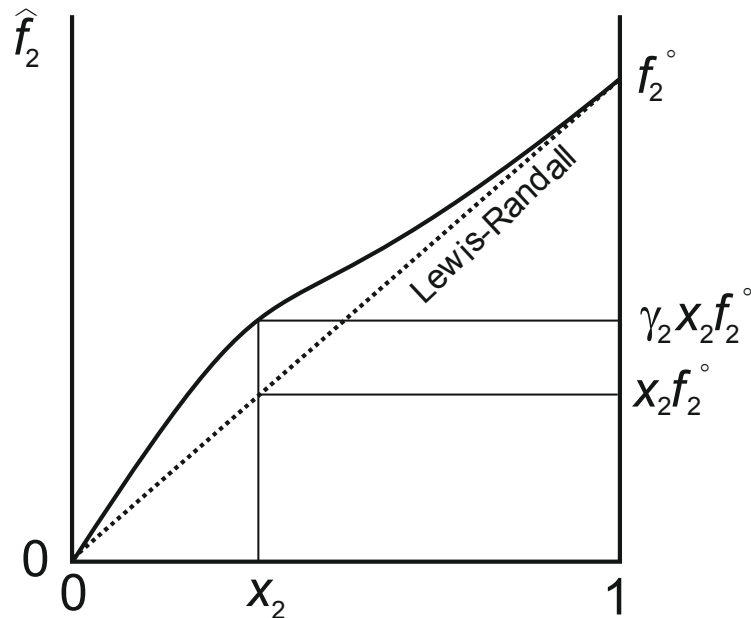
Standardno stanje – čista kapljevina pri temperaturi sustava i ravnotežnom tlaku

Iz definicije aktivnosti i koeficijenta aktivnosti: Ako je Poyntingov faktor  $\approx 1$

Realne otopine    Idealne otopine

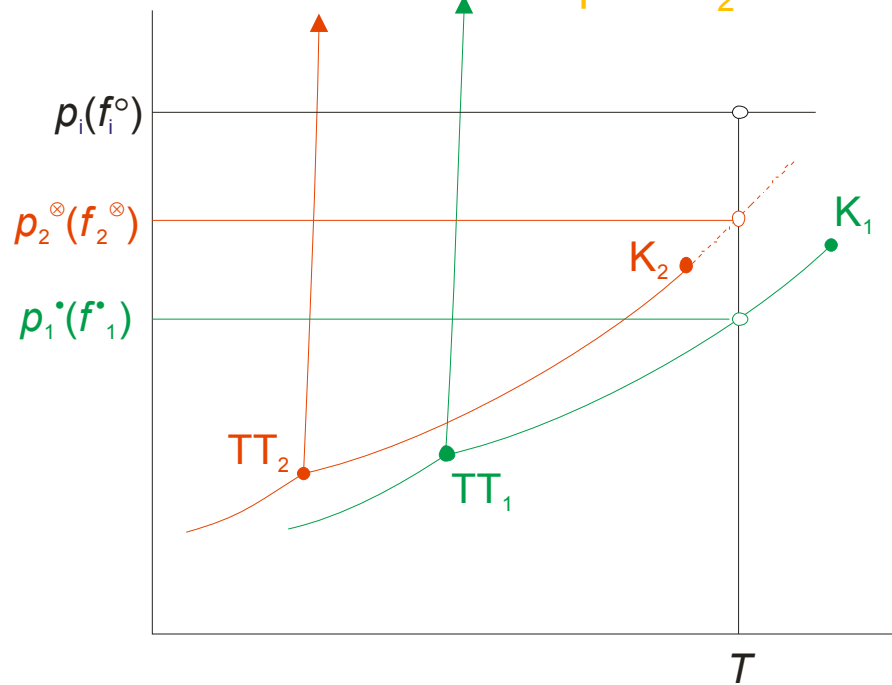
Ako je tlak nizak:  $f_i^\circ \approx f_i^\bullet = \varphi_i^\bullet p_i^\bullet \approx p_i^\bullet$

$$\hat{f}_i = \gamma_i x_i f_i^\circ \quad \hat{f}_i = x_i f_i^\circ \quad p_i = \gamma_i x_i p_i^\bullet \quad p_i = x_i p_i^\bullet \quad \hat{f}_i = \hat{\varphi}_i p_i \approx p_i$$

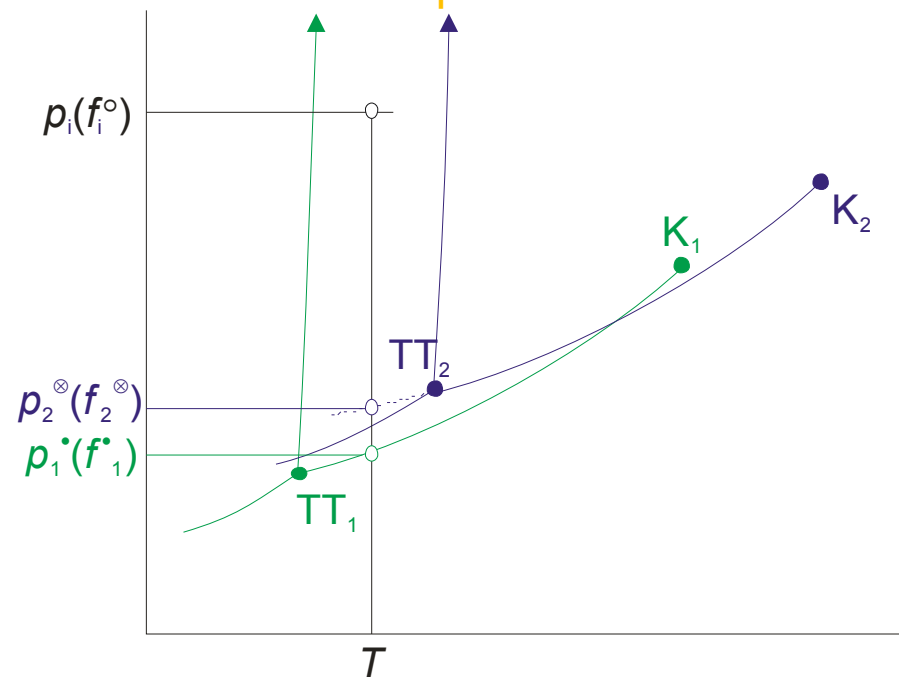


# Standardne fugacitivnosti komponenata u asimetričnim otopinama

Otopine plinova,  
Npr. CO<sub>2</sub> u toluenu



Otopine krutina,  
Npr. naftalen u toluenu



Ekstrapolacijski postupci

$$f_2^\circ = f_2^\bullet \exp\left(\frac{1}{RT} \int_{p_2^\bullet}^p v_2^L dp\right) \quad f_2^\circ = f_2^{\otimes} \exp\left(\frac{1}{RT} \int_{p_2^{\otimes}}^p v_2^{L\otimes} dp\right) \quad v_2^{L\otimes} = ?$$

# Otopine plinova ili krutina u kapljevina

Odstupanja od Henryjeva zakona  
za realne otopine

Henryjev zakon

$$p_2 = x_2 k_H$$

$$\hat{f}_2 = x_2 k_H$$

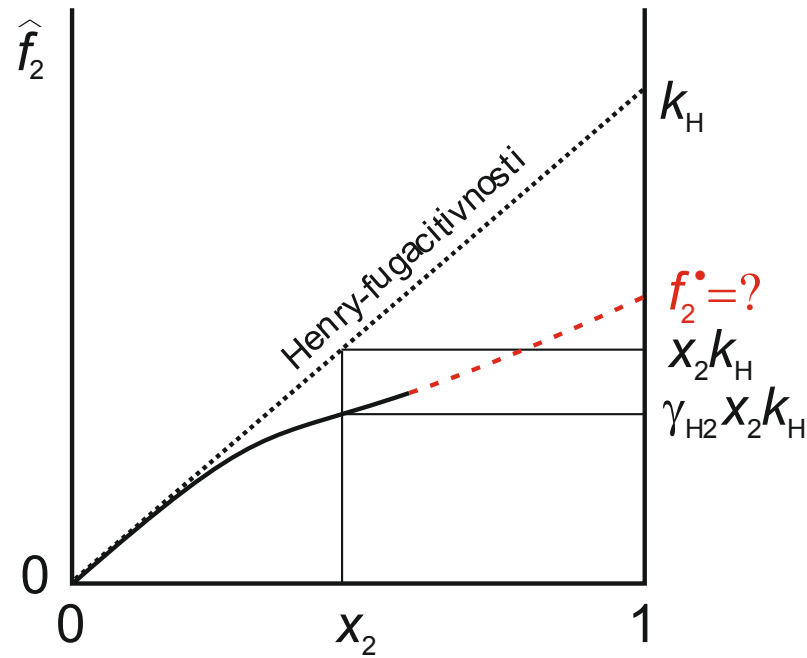
# Aktivnost otopljene tvari u asimetričnim otopinama

Realne otopine

$$\hat{f}_2 = \gamma_{H2} x_2 k_H$$

Idealne otopine

$$\hat{f}_2 = x_2 k_H$$

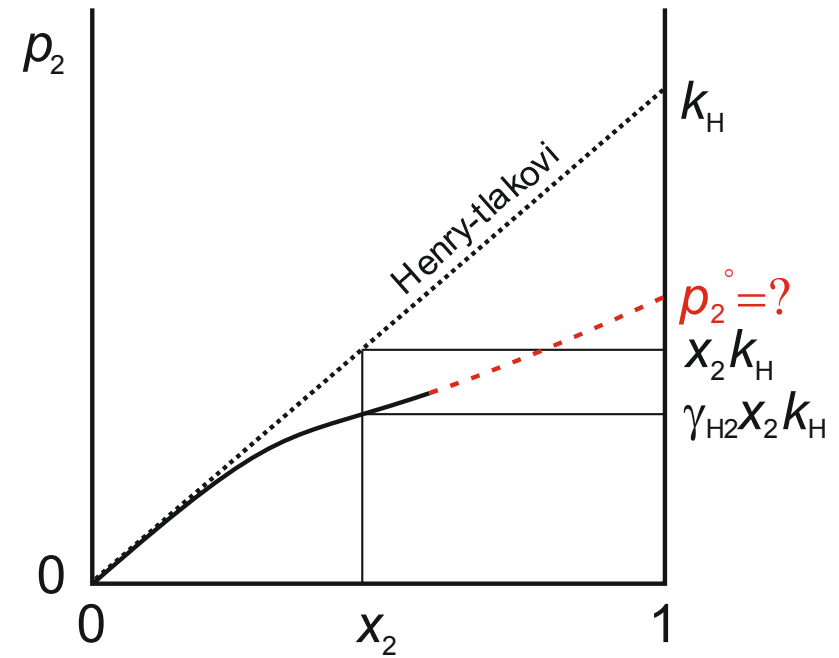


Realne otopine

$$p_2 = \gamma_{H2} x_2 k_H$$

Idealne otopine

$$p_2 = x_2 k_H$$



**NOVA DEFINICIJA IDEALNE OTOPINE !!!**



# Nova (asimetrična) definicija idealne otopine

- Otopina se vlada idealno u vrlo razrijeđenom području
- Parcijalna fugacitivnost (parcijalni tlak otapala) razmjernan je njegovu množinskom udjelu – slijedi Raoultov zakon
- Topljivost plina razmjerna je njegovu parcijalnom tlaku iznad otopine – slijedi Henryjev zakon
- Mikroskopski gledano, u idealnoj otopini otapanje molekula plina (ili krutine) ne remeti interakcije molekula otapala;
- Interakcije molekula otopljene tvari zanemarive su!

# Kemijski potencijal – parcijalna molarna Gibbsova energija

$$\mu_i = \bar{g}_i = \left( \frac{\partial G}{\partial n_i} \right)_{T, p, n_{j \neq i}}$$

Parcijalna molarna Gibbsova energija

Središnja veličina kemijsko inženjerske termodinamike

$$\mu_i = \left( \frac{\partial U}{\partial n_i} \right)_{S, V, n_{j \neq i}}$$

Jesu kemijski potencijali,  
ali nisu parcijalne molarne veličine  
(tlak i temperatura nisu konstantni)

$$\mu_i = \left( \frac{\partial H}{\partial n_i} \right)_{S, p, n_{j \neq i}}$$

$$\mu_i = \left( \frac{\partial A}{\partial n_i} \right)_{T, V, n_{j \neq i}}$$

# Promjena entropije pri idealnom miješanju iz kemijskih potencijala

$$g = x_1\mu_1 + x_2\mu_2$$

$$\mu_i = \mu_i^\circ + RT \ln a_i$$

$$\mu_i = g_i + RT \ln a_i$$

Standardno stanje –  
čista tvar

$$g^M = g - x_1g_1 - x_2g_2 =$$

$$= x_1(g_1 + RT \ln a_1) + x_2(g_2 + RT \ln a_2) - x_1g_1 - x_2g_2 =$$
$$= RT(x_1 \ln a_1 + x_2 \ln a_2)$$

$$g^M = RT \sum x_i \ln a_i$$

$$g^M = RT \sum x_i \ln(x_i \gamma_i) \quad \text{Veza aktivnosti i koeficijenta aktivnosti}$$

$$g^{M,\text{id}} = RT \sum x_i \ln x_i$$

Iz opće termodinamike

$$s^{M,\text{id}} = - \left( \frac{\partial g^{M,\text{id}}}{\partial T} \right)_p \quad s^{M,\text{id}} = -R \sum x_i \ln x_i$$

# Logaritam aktivnosti i logaritam koeficijenta aktivnosti kao PMV

Metoda odsječka za Gibbsovu energiju

OBRAZAC:  $v = \sum x_i \bar{v}_i$

$$\frac{g^M}{RT} = \sum x_i \ln a_i$$

$$\frac{g^{\text{ex}}}{RT} = \sum x_i \ln \gamma_i$$

$$h = \sum x_i \bar{h}_i$$

$$s^M = \sum x_i s_i^M$$

Logaritam aktivnosti i logaritam koeficijenta aktivnosti su PMV

